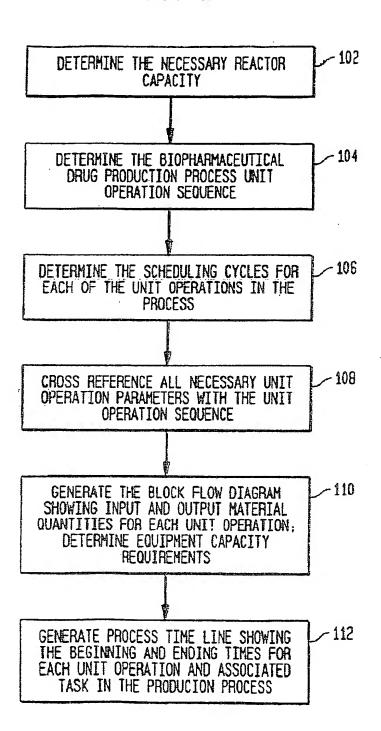
Title: The Use of Sub (Partial) Cycles, ...

Inventor: Peter G. Brown

FIG. 1

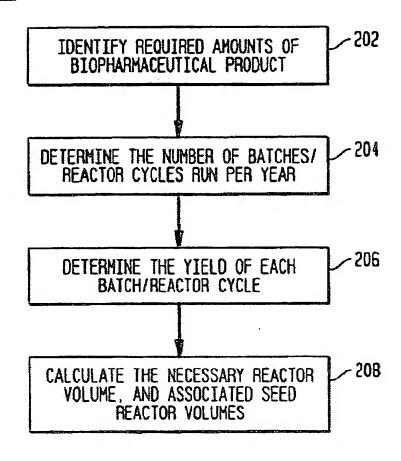


Title: The Use of Sub (Partial) Cycles, ...

Inventor: Peter G. Brown

FIG. 2

102



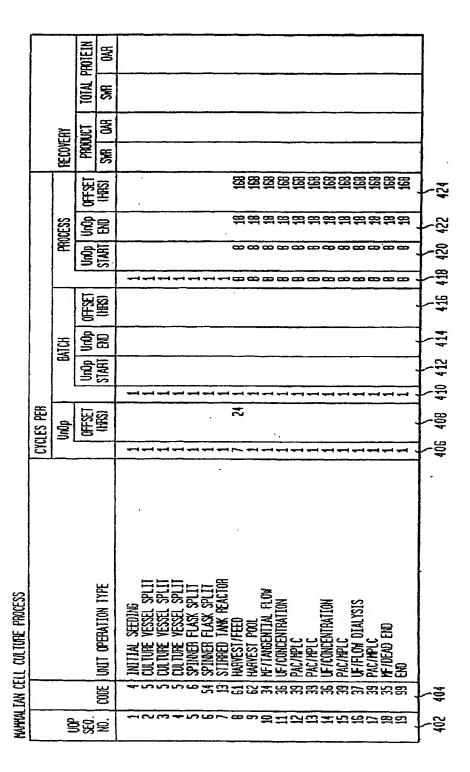
MICROBIAL FEDVENTATION PROCESS

1   INODIUM PREP   1   1   1   1   2   2   2   2   3   4   4   5   3   4   4   5   3   4   4   5   3   4   4   5   3   3   4   5   4   5   3   3   3   3   3   3   3   3   3	_		,			_
TOTALES FOR			<b>POTETIN</b>	\$	<u> </u>	- <u>25</u>
COUCE PCB   CHILD OPERATION TYPE   CYCLES PCB   CHICAGO   CHICAG			TOTAL P	<b>S</b>	\$	1 
COCC (NUI OPERATION TYPE  1 INOQUIAN PREP  2 ILAK GOMINE  3 SED FEBRUATION  3 FROME CIVILIA PREP  5 ILAK GOMINE  5 ILAK GOMINE		Ě	DUCT	88	2000 2000 2000 2000 2000 2000 2000 200	- <u>F</u>
1   1000 UN PREP   1   1   1   1   1   1   1   1   1	L	<b>E</b>	ш	Щ	1002 1002 1002 1002 1003 1003 1003 1003	]~¤
CODE UNIT OPERATION TYPE  1 INODULUM PREP  2 FLACK GROWTH  5.3 FLACK GROWTH  5.3 FLACK GROWTH  5.4 FLACK GROWTH  5.4 FLACK GROWTH  5.5 FLACK GROWTH  5.5 FLACK GROWTH  5.6 FLACK GROWTH  5.7 FLACK GROWTH  5.8 FLACK GROWTH  5.9 FLACK GROWTH  5.1 FLACK GROWTH  5.1 FLACK GROWTH  5.1 FLACK GROWTH  5.2 FLACK GROWTH  5.3 FLACK GROWTH  5.4 FLACK GROWTH  5.4 FLACK GROWTH  5.5 FLACK GROWTH  6.5 FLACK GROWTH  6.5 FLACK GROWTH  6.5 FLACK GROWTH  6.6 FLACK GROWTH  6.7 FLACK GROWTH  6.7 FLACK GROWTH  6.7 FLACK GROWTH  6.8 FROUGH CRITICAL HAPPEST  6.9 FROUGH CRITICAL HAPPEST  6.1 FLACK GROWTH  6.0			OFFSET	豎	· .	-25
1   NODULIN PREP   NODULIN PREP   1   NODULIN PREP   NODULIN PREP   1   NODULIN PREP   NODULIN PREP   1   NODULIN PREP   NODULIN PREP   1   NODULIN PREP   NODULIN PREP   1   NODULIN PREP   1   NODULIN PREP   1   NODULIN	ľ	OCESS				t
1   NOCULIN PREP   1   0   0   0   0   0   0   0   0   0		8-	g S	E SE		
1   NOCULIN PREP   1   0   0   0   0   0   0   0   0   0	l				पानी पानी पानी पानी पानी पानी पानी पानी	<b>上</b> 器
1   1000LUN PREP   1   3   1   518HT   ENCORE UNIT OPERATION TYPE   1   1   3   1   1   1   3   1   1   1			OFFSET	2		
1   100CULUN PREP   1   3   5   5   5   5   5   5   5   5   5		돌		1	22222	-≋
CODE UNIT OPERATION TYPE  1 INOCULUM PREP  2 RASK GROWTH  3 SEED FEPRENTATION  3 PRODUCTION FEBRENTATION  51 IEAT EXCHANGE  52 CONT. CENTRIFFOCATION/PRECEPTIATE HARVEST  53 IEAT EXCHANGE  54 IEAT EXCHANGE  55 IEAT EXCHANGE  56 CONT. CENTRIFFOCATION/PRECEPTIATE HARVEST  57 IEAT EXCHANGE  58 FEOUR CENTRIFFOCATION/PRECEPTIATE HARVEST  59 UL TRAFIL TRATION/PRECEPTIATE HARVEST  50 UL TRAFIL TRATION/PRECEPTIATE HARVEST  51 IEAT EXCHANGE  52 CONT. CENTRIFFOCATION PRIC  53 UL TRAFIL TRATION/PRECEPTIATE HARVEST  54 PRODUCT AUSORPTION PRIC  57 UL TRAFIL TRATION/PREAD END  58 PRODUCT AUSORPTION PRIC  59 FROUCT AUSORPTION PRIC  51 UTAFIL TRATION/PREAD END  51 ITAFIL TRATION/PREAD END  52 FROUCT AUSORPTION PRIC  53 PRODUCT AUSORPTION PRIC  54 PRODUCT AUSORPTION PRIC  55 FROUCT AUSORPTION PRIC  56 FROUCT AUSORPTION PRIC  57 UL TRAFIL TRATION/PREAD END  58 FROUCT AUSORPTION PRIC  59 FROUCT AUSORPTION PRIC  50 PRODUCT AUSORPTION PRIC  51 HAFFIL TRATION/PREAD END  52 FROUCT AUSORPTION PRIC  53 PRODUCT AUSORPTION PRIC  54 PRODUCT AUSORPTION PRIC  55 PRODUCT AUSORPTION PRIC  56 FROUCT AUSORPTION PRIC  57 PRODUCT AUSORPTION PRIC  58 PRODUCT AUSORPTION PRIC  59 FROUCT AUSORPTION PRIC  50 PRODUCT AUSORPTION PRIC  50 PRODUCT AUSORPTION PRIC  51 PRICE  52 PRODUCT AUSORPTION PRIC  53 PRODUCT AUSORPTION PRIC  54 PRODUCT AUSORPTION PRIC  55 PRODUCT AUSORPTION PRIC  56 PRODUCT AUSORPTION PRIC  57 PRICE  58 PRODUCT AUSORPTION PRIC  59 PRODUCT AUSORPTION PRIC  50 PRICE  50 PRICE  50 PRICE  50 PRICE  50 PRICE  50 PRICE  51 PRICE  51 PRICE  52 PRICE  53 PRICE  54 PRICE  55 PRICE  56 PRICE  57 PRICE  57 PRICE  58 PRICE  58 PRICE  59 PRICE  50 PRICE  51 PRICE  51 PRICE  51 PRICE  52 PRICE  53 PRICE  54 PRICE  55 PRICE  56 PRICE  57 PRICE  57 PRICE  57 PRICE  58 PRICE  58 PRICE  59 PRICE  50 PRICE  51 PRICE  51 PRICE  51 PRICE  51 PRICE  52 PRICE  53 PRICE  54 PRICE  55 PRICE  55 PRICE  56 PRICE  57 PRICE  57 PRICE  5		8	호	SIA	вове	
CODE UNIT OPERATION TYPE  1 INOCULUM PREP  2 RASK GROWTH  3 SEED FEPRENTATION  3 PRODUCTION FEBRENTATION  51 IEAT EXCHANGE  52 CONT. CENTRIFFOCATION/PRECEPTIATE HARVEST  53 IEAT EXCHANGE  54 IEAT EXCHANGE  55 IEAT EXCHANGE  56 CONT. CENTRIFFOCATION/PRECEPTIATE HARVEST  57 IEAT EXCHANGE  58 FEOUR CENTRIFFOCATION/PRECEPTIATE HARVEST  59 UL TRAFIL TRATION/PRECEPTIATE HARVEST  50 UL TRAFIL TRATION/PRECEPTIATE HARVEST  51 IEAT EXCHANGE  52 CONT. CENTRIFFOCATION PRIC  53 UL TRAFIL TRATION/PRECEPTIATE HARVEST  54 PRODUCT AUSORPTION PRIC  57 UL TRAFIL TRATION/PREAD END  58 PRODUCT AUSORPTION PRIC  59 FROUCT AUSORPTION PRIC  51 UTAFIL TRATION/PREAD END  51 ITAFIL TRATION/PREAD END  52 FROUCT AUSORPTION PRIC  53 PRODUCT AUSORPTION PRIC  54 PRODUCT AUSORPTION PRIC  55 FROUCT AUSORPTION PRIC  56 FROUCT AUSORPTION PRIC  57 UL TRAFIL TRATION/PREAD END  58 FROUCT AUSORPTION PRIC  59 FROUCT AUSORPTION PRIC  50 PRODUCT AUSORPTION PRIC  51 HAFFIL TRATION/PREAD END  52 FROUCT AUSORPTION PRIC  53 PRODUCT AUSORPTION PRIC  54 PRODUCT AUSORPTION PRIC  55 PRODUCT AUSORPTION PRIC  56 FROUCT AUSORPTION PRIC  57 PRODUCT AUSORPTION PRIC  58 PRODUCT AUSORPTION PRIC  59 FROUCT AUSORPTION PRIC  50 PRODUCT AUSORPTION PRIC  50 PRODUCT AUSORPTION PRIC  51 PRICE  52 PRODUCT AUSORPTION PRIC  53 PRODUCT AUSORPTION PRIC  54 PRODUCT AUSORPTION PRIC  55 PRODUCT AUSORPTION PRIC  56 PRODUCT AUSORPTION PRIC  57 PRICE  58 PRODUCT AUSORPTION PRIC  59 PRODUCT AUSORPTION PRIC  50 PRICE  50 PRICE  50 PRICE  50 PRICE  50 PRICE  50 PRICE  51 PRICE  51 PRICE  52 PRICE  53 PRICE  54 PRICE  55 PRICE  56 PRICE  57 PRICE  57 PRICE  58 PRICE  58 PRICE  59 PRICE  50 PRICE  51 PRICE  51 PRICE  51 PRICE  52 PRICE  53 PRICE  54 PRICE  55 PRICE  56 PRICE  57 PRICE  57 PRICE  57 PRICE  58 PRICE  58 PRICE  59 PRICE  50 PRICE  51 PRICE  51 PRICE  51 PRICE  51 PRICE  52 PRICE  53 PRICE  54 PRICE  55 PRICE  55 PRICE  56 PRICE  57 PRICE  57 PRICE  5					mmmmmmmmnonoommeemmeemmee .	누읆
CODE LINIT OPERATION TYPE  1 INOCULUN PREP  2 FLASK GROWTH  3 SEED FEMENTATION  3 INOCULUN PREP  53 SEED FEMENTATION  51 IKAI EXCHANGE  60 CMT. CENTRIPOLATION/MICHE CELL HARVEST  61 ICAI CENTRIPOLATION/PRECIPITATE HARVEST  62 CMT. CENTRIPOLATION/PRECIPITATE HARVEST  63 ICAI CENTRIPOLATION/PRECIPITATE  64 RESUSPENSION/SUFFACTANT  65 CMT. CENTRIPOLATION/PRECIPITATE  65 CMT. CENTRIPOLATION/PRECIPITATE  66 CMT. CENTRIPOLATION/PRECIPITATE  67 UTAFIL TRATION/ICAN PRIC  68 PRODUCT ADSORPTION PRIC  68 PRODUCT ADSORPTION PRIC  69 FROUCT ADSORPTION PRIC  60 TRAFIL TRATION/ICAO END  60 PRODUCT ADSORPTION PRIC  60 TRAFIL TRATION/ICAO END  60 PRODUCT ADSORPTION PRIC  60 TRAFIL TRATION/ICAO END  61 TRAFIL TRATION/ICAO END  62 FROUCT ADSORPTION PRIC  63 TRAFIL TRATION/ICAO END  64 FROUCT ADSORPTION PRIC  65 PRODUCT ADSORPTION PRIC  66 FROUCT ADSORPTION PRIC  66 FROUCT ADSORPTION PRIC  67 TRAFIL TRATION/ICAO END  68 FROUCT ADSORPTION PRIC  67 TRAFIL TRATION/ICAO END  68 FROUCT ADSORPTION PRIC  68 FROUCT ADSORPTION PRIC  69 FROUCT ADSORPTION PRIC  60 TRAFIL TRATION/ICAO END  60 FROUCT ADSORPTION PRIC  60 TRAFIL TRATION/ICAO END  60 FROUCT ADSORPTION PRIC  61 TRAFIL TRATION/ICAO END  62 TRAFIL TRATION/ICAO END  63 TRAFIL TRATION/ICAO END  64 TRAFIL TRATION/ICAO END  65 TRAFIL TRATION/ICA	LES PER	gur Gur	OFFSET	€		5
CODE UNIT OPERATION TYPE  1 INOQULUM PREP 2 FLASK GROWIH 3 SEED FEMENTATION 3 PRODUCTION FEMENTATION 51 HEAT EXCHANGE 60 CMT. CENTRIFUGATION/MICH PRESSURE 51 HEAT EXCHANGE 51 HEAT EXCHANGE 52 COMT. CENTRIFUGATION/PRECIPITATE HAPVEST 6EL DISARPTION/HIGH PRESSURE 53 HEAT EXCHANGE 6EL DISARPTION/HIGH PRESSURE 54 HEAT EXCHANGE 55 HEAT EXCHANGE 6EL DISARPTION/HIGH PRESSURE 6EL DISARPTION/HIGH PR	D.S	_ ,			प्रानं कर्मों कर्मा कर्म कर्म कर्म कर्म कर्म कर्म कर्म कर्म	~ <u>8</u>
			APPLICATION OF THE PROPERTY OF	UNIT OPERATION TYPE	5× 55 55 55 55 55 55 55 55 55 55 55 55 5	
\$25 47 47 67 80 8 1 3 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1			į	ğ		304
		<u>a</u>	( <b>)</b>	2	またろすららてほり加は江北田村広は打印的の力な力	305

Title: The Use of Sub (Partial) Cycles, ...

Inventor: Peter G. Brown

FIG. 4
UNIT OPERATIONS

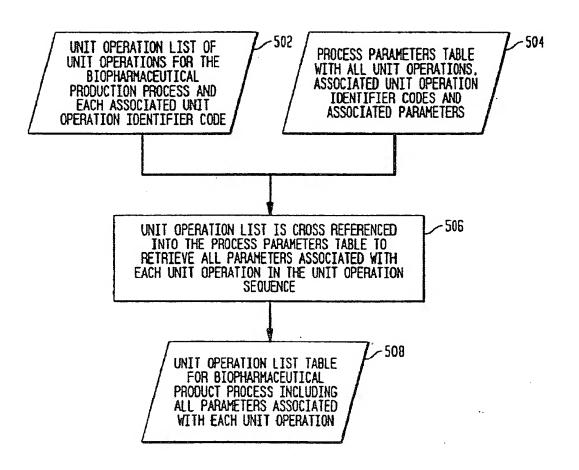


Title: The Use of Sub (Partial) Cycles, ...

Inventor:

Peter G. Brown

FIG. 5



Title: The Use of Sub (Partial) Cycles, ...
Inventor: Peter G. Brown

# FIG. 6A

UNIT OPERATION ID CODE	UNIT OPERATION TYPE	PARAMETERS .
ı	INOCULUM PREP	e of Flasks, volume of Flasks, itemperature, astitation, duration, final oo
2	FLASK EROYTH	SCALE UP RATIO, MEDIA VOLUME, TEMPERATURE, ASTITATION, DURATION, FIHAL CO
3	FEFRENTATION SEED	SCALE UP RATTO, FERNENTOR WORKING VOLUME, ANTIFORM, BASE ACID, GROW TEMPERATURE, ACTIVATION, SPARGE RATE, BACK PRESSURE, TOTAL OURATTOR
ł	FERMENTATION PRODUCTION	SCALE UP RATTO, GENERIOR NORKING VOLUME, ANTIFOAN A, ANTIFOAN B, BASE, ACID, GROW TEMPERATURE, AGITATION, SPARSE RATE, BACK PRESSURE, TOTAL OURATION, FINAL OK, DRY CELL HASS, PRODUCT CONCENTRATION, CIP, SIP
5	HEAT EXCHANGE	PROCESS INITIAL & FINAL TEMP: UTILITY INITIAL & FINAL TEMP: PROCESS SPECIFIC HEAT: Design type, step recovery of product, step recovery of t.p., temperature regulation, c.p., s.p
8	BATCH CENTRIFYCATION	SYSTEM VOID VOLUME, RCF., TIDE., VOLUME REDUCTION, VASH VOLUME, CLEAR, RIAGE
7	RESOLUBLIZATION RESUSPENSION	REAGENT/PRODUCT RATIO, TITRATION SOLUTION, RESOLUBLIZATION, ASITATION, SOLUTION NAVE, STEP RECOVERY OF THE PRODUCT, STEP RECOVERY OF T.P., TENFERATURE PEGULATION, CIP, SIP
8	CELL DISRUPTION HIGH PRESS. HUMHOGENIZATION	PRODUCT TERMERATURE, UNILLITY TEMPERATURE, VOID VOLUME, MARKER OF PASSES, PRESSURE, FLOW RATE, TEMPERATURE INCREASE, WASH, RINSE, STEP RECOVERY OF PRODUCT, STEP RECOVERY OF T.P., TEMPERATURE REQUIATION, CIP
9	DILUTE ALIH 278£VLIVIL	REASENT PRODUCT RATIO, THRATION SOLUTION, DILUTION HIME, ASTIATION, SOLUTION NAVE SIEP RECOVERY OF PRODUCT, STEP RECOVERY OF T.P., TEMPERATURE REGULATION, CIP. SIP
10	BATCH CENTRIFUGATION PRECIPITATE HARVEST	SYSTEM VOID VOLUME, ROF, TIME, VOLUME REDUCTION, WASH VOLUME, CLEAN, RIDNE, STEP RECOVERY OF PRODUCT, STEP RECOVERY OF T.P., TEMPERATURE REGULATION, CIP, SIP
11	LEZYZHAD ATTH CHAOTRONE	REAGENT/PRODUCT RATIO, TITRATION SOLUTION, RESOLUBLIZATION, ASTRATION, SOLUTION NAME, STEP RECOVERY OF PRODUCT, STEP RECOVERY TO TP., TEMPERATURE REGULATION, CIP., SIP
-	•	•

Title: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown

# FIG. 6B

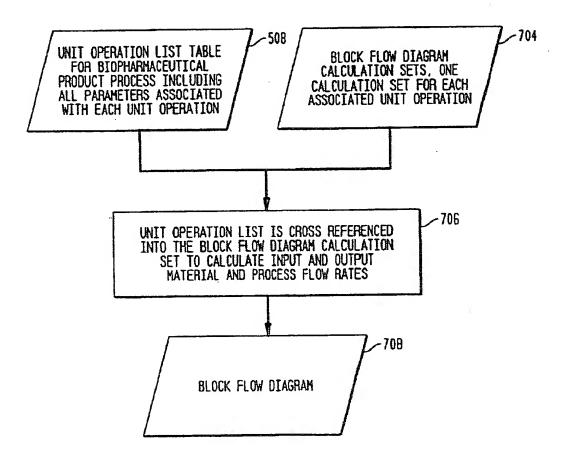
504

SOLUTION TYPE	TASKS	TASK DURATION
S-101	SETUP, PREINCUBATION, Incubation, Clean up	3, 3, 23, .3, HRS
S-101	SETUP, PREINCURATION, Incuration, Clean up	1, 1, 23, .3, HRS
S-101, 102, 103, 104, 105	SETUP. PREINCURATION, PERMENTATION, NARYEST, CIP. SIP, CLEAN UP	1, 1, 21, .5, 1, 1, 3 HPS
\$-101, 102 103, 104, 105	SETUP, PREINCUBATION, Permentation, CIP, SIP, Clean up	•
	SETUP, TRANSFER, CIP, SIP, CLEAN UP	•
S-106	SETUP, CENTRIFUGATION, WASH, CIP, SIP, CLEANIP	•
S-107	SETUP, DILUTION, AGITATE, CIP, SIP, CLEAN UP	•
S-107	SETUP, LYSIS. CIP, SIP, CLEAN UP	•
S-108	SETUP. DILUTION, AGITATE, CIP, SIP, CLEAN UP	•
\$-108	SETUP, CENTRIFICATION, WASH, CIP, SIP, CLEAN UP	-
S-103	SETUP, FLUSH, PRIME, CONCENTRATION, DILUTION, WASH, FLUSH, STORE, CIP, SIP, CLEANUP	•
•	•	•

Title: The Use of Sub (Partial) Cycles, ...

Inventor: Peter G. Brown

FIG. 7



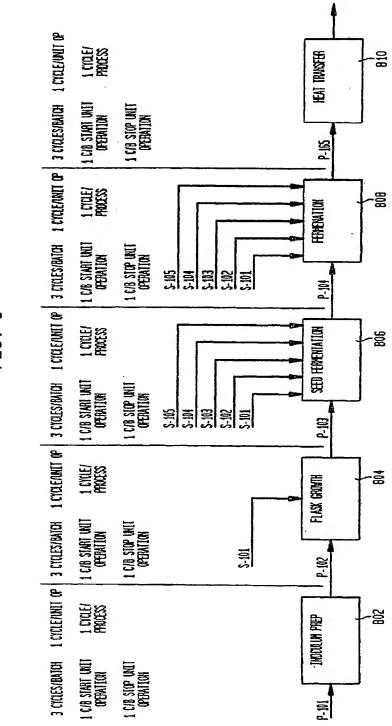


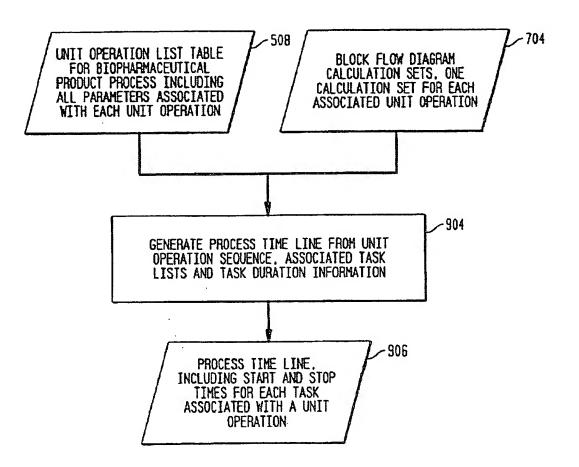
FIG. 8

Title: The Use of Sub (Partial) Cycles, ...

Inventor:

Peter G. Brown

FIG. 9



Title: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown

FIG. 10

## SAMPLE APPLICATION OF PROCESS DESIGN CYCLES IN PROCESS SCHEDULING

KICROBIAL FERMENTATION PROCESS (SEE )	INIT OPERATION LISTI		
		FIRST PROCESS CYCLE	SECOND PROCESS CYCLE
	DURATION	AEEK DYA	WEEK DAY
NOTE: NONE OF THE UNIT OPERATIONS IN ISEE UNIT OPERATION 8 IN THE NAMALI	THIS PROCESS HAVE NOTE AN CELL CULTURE PROCESS I	THAT 1 CYCLE PER UNIT OPERATION FOR AN EXAMPLE OF MULTIPLE CYCLE	S PER UNIT OPERATION
UNIT OPERATIONS 1-6 UNDERSO THREE RE THIS TRANSLATES TO THREE RUNS ON A F ASSOCIATED WITH EACH FERNENTOR RUN	ERMENTOR WITH EACH HARVE LUNET OP 41 ARE THE PREVI	CT HAND OP SEED BEING SHIFED	HUR MILLENG AL LINIT LIP /
A / 10 FTTMEDITATION OF OUR CONCESS DATE	ITU .		
4 PRODUCTION FERVE 5 HEAT EXCHANGE 6 CENTRIFUGATION	VTATION 24 HRS 1 HR 1 HR	1 FRI - SAT 2 SAT - SUN 2 SUN - MON 2 MON - TUE 2 TUE 2 TUE	3 MON - TUE 3 Tue 3 Tue
2/3 FERNENTATION CYCLES PER BA' 1 INOCALUM PREP 2 Flask Growth	TCH 24 HRS 24 HRS	2 Sun - Hon 2 Hon - Tue	3 SUN - HON 3 HON - TUE
3 SEED FERMENTAION 4 PRODUCTION FERME 5 HEAT EXCHANGE	24 HRS HTATION 24 HRS 1 HR	2 Sun - Mon 2 Mon - Tue 2 Tue - Wed 2 Med - Thu 2 Thu 2 Thu 2 Thu	3 IVE - YEU 3 YED - THU 3 THU 2 THU
3/3 FERMENTATION CYCLES PER BA 1 INDOCULUM PREP			
2 Flask Growth 3 Seed Fermentaion 4 Production Ferme	24 HRS 24 HRS NTATION 24 HRS	2 YEU - IHU 2 THU - FRI 2 FRI - SAT	3 TRU - TRU 3 TRU - FRI 3 FRI - SAT
5 HEAT EXCHANGE 6 CENTRIFUGATION UNIT OPERATION 7 POOLS THE HARVESTS	1 HR 1 HR FROM THE THREE FERMENTA	2 TUE - VED 2 YED - THU 2 THU - FRI 2 FRI - SAT 2 SAT 2 SAT TION CYCLES ABOYE 3 KON	3 SAT
7 POOL HARVESTS UNIT OPERATIONS 8-9 UNDERGO THREE F THIS TRANSLATES TO THREE CONSECUTIV (UNIT OP 8 & 10) AT THE INLET AND 1	EPETATIVE CYCLES PER BAT F PASSES THROUGH CELL DI	CH AS SET BEFORE CONTINUING WITH SPUPTOR (UNIT OP 9) WITH ITS ASS	4 NON UNIT OPERATION 11 OCIATED HEAT EXCHANGERS
1/3 DISPUPTION CYCLES PER BATO 8 HEAT EXCHANSE 9 CELL DISPUPTION	Ж		
10 HEAT EXCHANGE 2/3 disruption cycles per bati 8 heat exchange	0.5 HR CH	3 HON	4 HON
9 CELL DISPUPTION 10 HEAT EXCHANGE 3/3 DISPUPTION CYCLES PER BAT		3 HON	4 MON
8 HEAT EXCHANGE 9 CELL DISPUPTION 10 HEAT EXCHANGE	0.5 HB	3 MON	4 MOH

Title: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown

## FIG. 11

### SAMPLE APPLICATION OF PROCESS DESIGN CYCLES IN PROCESS SCHEDULING

HICROBIAL FERMENTATION PROCESS (SEE UNIT (	PERATION LISTI		
		FIRST PROCESS CYCL	E SECOND PROCESS CYCLE
	CURATION	WEEK DAY	AEEK DAA
UNIT OPS 11-12 UNDERSO TWO REPETATIVE CY THIS TRANSLATES TO TWO CYCLES OF RESUSPE SURFACTANT AND RECONCENTRATING THE INSOL 1/2 PRODUCT VASHING CYCLES PER BATCI	VOING THE CELL TYSATE FROM JBLE PRODUCT TO A PASTE BY	THE CELL DISPUPTOR	
11 RESUSPENSION 12 CENTRIFUGATION 2/3 PRODUCT VASHING CYCLES PER BATC	0.5 HR 1 HR	3 NON 3 NON	4 HON
11 RESUSPENSION 12 CENTRIFUGATION UNIT OPS 13-22 UNDERGO ONLY ONE CYCLE PE	0.5 HR 1 HR	3 MON 3 MON E END OF THE PROCES	4 MON 4 MON S
13 RESUSPENSION 14 BUFFER EXCHANCE 15 FILTRATION 16 LIQUID CHROHATOGRAPHY 17 LIQUID CHROHATOGRAPHY 18 BUFFER EXCHANGE 19 LIQUID CHROHATOGRAPHY 20 BUFFER EXCHANGE 21 LIQUID CHROHATOGRAPHY 22 FILTRATION	0.5 HR 2 HR 2 HR 16 HRS 4 HRS 2 HRS 2 HRS 2 HRS	3 MOH 3 MON 3 MON 3 MOH - TUE 3 TUE 3 TUE 3 VED 3 VED 3 VED 3 VED 3 VED 3 VED	4 KON 4 KEN 4 KON - TUE 4 TUE 4 TUE 4 KED 4 KED 4 KED 4 KED 4 KED

		PROCESS TIME LINE	E	FUE													٦
		DURATION (HES.)	墨声	Γ	E .	RE. TDE SCALE (HRS)		ABS. DAYS		STARI		FINISH					
	OPERATION	CALC. AND	冒	- F	皇	DEE.	COPPL.	STARI	23	OHE H	1116	CATE	邕		ALCULATIONS		
Τ						15.5				06/03/96 08:00	08:00 AH						Т
	1 A INDCULUM PREP																
- m	SET UP	0.5		33.5	S. S.			<b>8</b> 5	25.52	36/69/36	63:30 AE	06/03/96	222				
ح الدا و	INCUATION CIFAN IP	200	200	32.5	3	38.5	<b>8</b>	88	85	06/03/96 03:30 P	E.E.	PH 05/0/36	25.39 25.55 37.57 37.57				
~ ~		3.0		29.0 HBS		8.5											
- 60 -	2 A FLASK GROWTH																
7 =		6	0.0	5.	25.5			25.5	988	96/10/90	23.3	96/10/90	88				
===	PREINCUBATION Incubation	30.0	0.0		<del>∑</del>	61.5		<u> </u>	385	87478 967478 967478	25.30 25.30 25.30 26.30	96/00/96					
#		0.3	ᆰ	S S S			8.39	1	2	5/3	S	8/03/8	욃				T
==		75.0		25.0 配		61.5											
<del></del>	3 A SED FERENTATION																
250		2.5			82			æ.5.	25.5	96/05/3 96/05/3	# 30 F	6 11:30 AN 06/05/36 1	12:30 13:30 13:30				
92	FERENTATION	12.			?	25.5		:55:	; <del></del>	86/05/9	01:30 P. 30 P. 30	96/96/96	R		10 1 Du	0 CO 100	ğ
ನನ		2.5				<u>=</u>	83.5		200	8790 190 190 190 190 190 190 190 190 190 1		96/96/98	38	) ? ?	50 7.	3.	3
~		3.00.0		3.5 8.8 8.8 8.8 8.8	•		99 25.55	3.5	3.52	06/06/36 06/06/36	12:30 A	86/96/90 96/96/90					
ನ್ನ	SUBIOTAL	28.5		28.5 HPS		83.0											
3		1	1	1	1	1	T										T

-					- 1.00 HRS					5.5 5.25 5.35				-	15
					9.4 LPM				9.4 LPH	<u>55</u>					~
_					582.119	2 <b>2</b> E			N 562.1 U	20.0 20.0 20.0 20.0 20.0 20.0 20.0 20.0	五石			ææ	
		10:00 AH 10:00 AH 10:00 AH 12:00 AH			08:30 A 09:00 A	3000 3000 3000 3000 3000 3000 3000 300			88	\$ 7. \$ 8. 8 8.	공동 보드				<b>=</b>
-		AN 06/07/96 AN 06/07/96 AN 06/07/96 AN 06/07/96 AN 06/07/96			AN 06/07/96 AN 06/07/96	M 06/07/96 11:00 AM 06/07/96 01:00 AM			06/07/36	96/0/36 96/0/36	AN 06/07/96 AN 06/07/96			0.50 06/03/96 01:30 PM 06/03/96 02:30 0.55 p6/03/96 02:30 PM 06/03/96 03:30	EE /
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-ZA-					<b>XX</b>	29.5			# C	2.2	7.5			_	~
FIG. 12A-2						6.79 .66			# # # # # # # # # # # # # # # # # # #		2.5			8.9	<b>,</b>
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•	4 A PRODUCTION FERRENTATION	SET UP PREINCOBATION FEIVENTATION CIP SIP CLEAN UP		5 A HEAT EXCHANCE		CLFA (P		6 A CONT. CENT./SOLIDS		NASH GID		SUBIDIAL	1 B INDCULUR FREP	SET UP	
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		E CALCALATIONS		ææ.			222			<b>左</b> 左	AN 50.0 L 1.7 UPK • 0.50 HZ	₹₹₹			***
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	F	11)	06/03/96 08:00 AM	06/03/96   03:30   PN   06/04/96   06/04/96   02:30   PN   06/04/96			6 06/04/36 12:30 PM 06/04/36 00 06/04/36 00 06/04/36 00 06/04/36 00:30 PM 06/05/36 0			11:30 12:30 14:30		23.30 A			885
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		OPERATION		2 C FLASK GROWTH	SET UP PPETIKUBATION		SUBTOTAL	3 C SEED FERENTATION				SIP CLEAN UP	SUBTOTAL	1 C PRODUCTION FEBRUATION			SIP	
				92	333	22	222	223	38	協切	## E	186	88	豆۔	388	35	325	3

	00 AM 06/07/95 08:30 AM 562.1 LP 9.4 LPM · 1.00 NFS 00 AM 06/07/95 10:00 AM 562.1 LP 9.4 LPM · 1.00 NFS 00 AM 06/07/95 11:00 AM 06/07/95 11:00 AM			08:00 AN 06/07/36 08:00 AN 562.1 LP 9.4 LPN • 1.00 16S 10:00 AN 562.1 LPN • 1.00 16S 10:00 AN 06/07/36 10:00 AN 1.0 LP 0.2 LPN • 0.10 16S 10:00 AN 06/07/36 10:21 AN 20.0 LPN • 0.25 HPS 10:21 AN 06/07/36 11:21 A	10:00	19:06 AN 06/07/96 10:06 AN 46.7 LP 1.6 LPM = 0.50 HBS 10:36 AN 06/07/96 11:36 AN 46.7 LP 1.6 LPM = 0.50 HBS 11:36 AN 06/07/96 12:36 PM 2:36 PM 06/07/96 02:36 PM 06/07/96 12:36 PM 06/07/96 12:36 PM 06/07/96 12:36 PM		
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FIG.	0.0.00			4.00	r: //	9.89. 9.03.99. 9.03.99.	<u>-</u>	
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	S C HEAT EXCHANCE SET UP TRANSFER CIP SIP CIEAR UP		6 C CONT. CENT./SOLIDS	SET UP CONTRIPOSATION WASH C.IP S.IP		7 A RESOLUBLIZATION SET UP DILUTION AGITATE CIP SIP CIFAN UP		8 A FEAT EXCHANGE
		. ₹5 £	i iği	4	<b>₹ ₹ £</b>			<u> </u>

Title: The Use of Sub (Partial) Cycles, ...

Inventor:

Peter G. Brown

0.30 FBS æ. €. 0.69 3.8 藍 S 66.5 !! 66.5 W 69.01 **EEEE ₹EEEE** EEEEE 4.54 06/07/36 12:52 PM 06/07/36 12:52 PM 뽈 96/20/90 96/20/90 96/20/90 96/20/90 367/0/30 367/0/30 367/0/30 367/0/30 86666 黑 2252 经费益的 222E EEEEE 855555 22222 22222 22222 8 ë 96/10/90 96/10/90 96/10/90 96/10/90 06/07/96 06/07/96 06/07/96 06/07/96 20198 10198 10198 10198 불 HAIS **නුනුන්න්** <u> अस्त्रस्य</u> 霱 DAYS <del>4</del> <del>4</del> <del>8</del> 8 8 8 £.5. START BS. 33 موموم 999 **EEE** SCALE 107.9 8 EXEC.  $\cong$ 寰 8 8 豐 黑 5  $\geq$ = 寰 鼍 0.5 FEE 0.0 STATE O.0 O.0 STATE O.0 O.0 STATE O.0 O.0 STATE O.0 ST 嵳 ₹ 8 2 **E** <u>=</u> 00000 00000 AM 00000 **DURATION** PROCESS KB355 SE 000 88000 <u>6.9</u> 9 A HOYMOGENIZATION OPERATION 10 A HEAT EXCHANCE 8 B HEAT EXCHANGE SET UP TRANSFER SIP CLEAN UP 9 낽 

FIG. 12D-

107.95 12.52 PH 06/07/95 01.10 PM 66.5 LP 3.7 LPH • 0.30 10/195 01.10 PM 06/07/95 01.51 PM 06/07/95 02.09 PM 06/07/95 02.27 PM 06/07/95 02		₩	<u> </u>		2	?				5	2			ī	۶	2		_
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Title: The Use of Sub (Partial) Cycles, ...

Inventor:

Peter G. Brown

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Title: The Use of Sub (Partial) Cycles, ...

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Inventor: Peter G. Brown

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Title: The Use of Sub (Partial) Cycles, ...

Inventor: Peter G. Brown

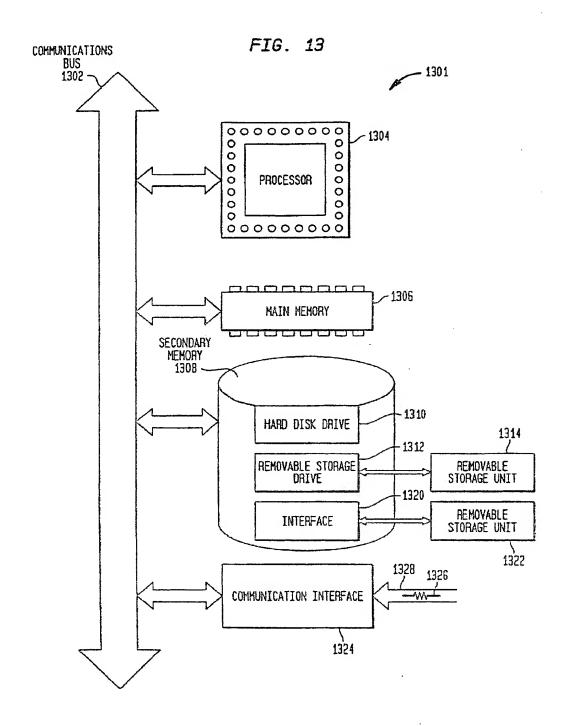


FIG. 14A

		710. 1	7/1	
				CROUP 1
-	UNIT OPERATION TYPE	PARAMETER	SOLH	
Īi	INNOCULUM PREP	MUNSER OF FLASKS HEDIA VOLUNE/FLASK		0.25 · LITERS
12	FLASK GROWTH	SCALE UP RATIO NEDIA VOLUNE/FLASK		10 FOLD 1.25 L
13	PRODUCTION	SCALE UP RATIO FERNENTOR NORKING VOLUNE ANTIFOAN A ANTIFOAN B BASE ACID	S-101 S-102 S-103 S-104 S-105	1 MI/L 1 MI/L 5 MI/L
14	INITIAL SEEDING	NUMBER OF AMPULES YOUNG PER AMPULE STARTING CELL DENSITY AMPULE SPLIT RATIO CULTURE YESSEL TYPE FEED YOUNG		2 2 MI 300,000 CELLS/MI 1 VESSELS/AMPULE ROLL. BOT. 100 MT
15	CULTURE VESSEL SPLIT	YESSEL SPLIT RATIO NEW YESSEL TYPE FFED VOLUME SERUM CONTENT		2 FB 100 MI 2.0% FETAL BOYINE SERUM
16	SPINNER FLASK SEEDING	FLASK FEED VOLUME VESSEL/FLASK RATIO UCAPRIER DENSITY MUMBER OF PRS WASHES IMMBER OF MEDIA WASHES NO. OF MEDIA/SERUM WASHES		4 LITERS 0.1 L. CELLS/L FLASK 5 Ga/LITER 2 1 2 FBS
17	BIOSYNTHESIS BIOPEACTOR PREPARATION ISTIRPED TANK PEACTORI	REACTOR FEED YOUNE SPINNER/REACTOR RATIO UCAPPLIER DENSITY MARBER OF PRS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERUH WASHES		500 LITERS  0.3  5 Ge/LITER  1 2
TØ	BIOSYNTHESIS Bioreactor Preparation (Holloy Fiber Reactor)	REACTOR FEED VOLUME MANBER OF PRS WASHES MANBER OF HEDIA WASHES MO. OF MEDIA/SERRH WASHES SERUM CONTENT		100 LITERS 2 2 2 2 2 2.0% FETAL BOVINE SERUM
T9	BIOSYNTHESIS BIOREACTOR PREPARATION (FLUIDIZED BED REACTOR)	PEACTOR FEED VOLUME UCAPRIER DENSTIY NUMBER OF PBS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERIM WASHES SERIM CONTENT		LITERS Gas/L
110	INITIAL SEEDING	MARBER OF AMPULES YOLUME PER AMPULE STARTING CELL DENSITY AMPULE SPLIT RATIO		2 2 MI 300,000 CELLS/MI 1 YESSELS/AMPULE

FIG. 14B

<u></u>	20UP 2		5	ROUP 3	
PARAMETER	SOLN.		PATAKETER	SOLH.	
TERPERATURE AGITATION DURATION		37 C 200 RPH 18 HOURS	FINAL CO		12
TEMPERATURE AGITATION DURATION		37 C 200 Hours 16 RPN	FINAL OO		12
GROWTH TEMPERATURE AGITATION SPANGE RATE BACK PRESSURE TOTAL DURATION		37 HOURS 1 HP/100L 1.5 YYH 5 PSIG 21 HRS	FINAL OO DRY CELL HASS PRODUCT CONCENTRATION CIP		12 9.96 Gos TDCH/L 0.3 Gas PRODUCT/L Y
SERIA CONTENT FEED RATE DAYS TO CONFLUENCE		2.0% FETAL BOYINE SERIAN 1 FEED PER VESSEL PER 2 Days 2 Days	APPLIFICATION FACTOR		100%
FEED RATE DAYS TO CONFLUENCE		1 FEED PER VESSEL PER 2 Days 2 Days	APPLIFICATION FACTOR		100%
SERIM CONTENT FEED RATE DAYS TO CONFLUENCE		2.0% FETAL BOVINE SERIM 1 FEED PER VESSEL PER 2 DAYS 2 DAYS	AMPLIFICATION FACTOR		100%
SERUM CONTENT FEED NATE  DAYS TO CONFLUENCE SERUM FREE MEDIA WASHES		2.0% FETAL BOVINE SERUM 1 FEED PER VESSEL PER 2 DAYS 10 DAYS 2	PRODUCT CONCENTRATION TOTAL PROTEIN CONCEN.		2500% Hg PROD/L 0.125 Hg TP/HI
MARBER OF REACTORS FEED RATE DAYS TO CONFLUENCE		1 FEED PER VESSEL PER 1 DAYS 10 DAYS	HARYEST YOLUNE PRODUCT CONCENTRATION TOTAL PROTEIN CONCEN.		500% LITERS 25 Hg PROD/L 0.125 Hg TP/HI
NUMBER OF REACTORS FEED RATE DAYS TO CONFLUENCE		1 FEED PER VESSEL PER 1 DAYS 10 DAYS	PRODUCT CONCENTRATION TOTAL PROTEIN CONCEN.		2500% Hg PROD/L 0.125 Hg TP/MI
SERUM CONTENT FEED RATE Days to confluence		2.0% FETAL BOYINE SERVING 1 FEED PER VESSEL PER 2 DAYS 2 DAYS	AMPLIFICATION FACTOR		100%

Title: The Use of Sub (Partial) Cycles, ...
Inventor: Peter G. Brown

FIG. 15A

_		F16	LJA		
	INTER ACCULTANT AND	01011-000		FROUP 1	
	UNIT OPERATION TYPE	PARWETER	SOU1.		
		CULTURE VESSEL TYPE FEED VOLUME		ROLL. BOT. 100	MI
T11	CULTURE VESSEL SPLIT	SEURI CONTENI NEA AEZZET LIDE NEA AEZZET LIDE		2 RB 100 2.0%	NI Fetal Boyine Serlm
112	SPIINER FLASK SPLIT	PLASK FEED VOLUME VESSEL/PLASK RATIO UCAPRIER DENSITY NAMEER OF PES VASIES NAMEER OF MEDIA VASIES NO. OF MEDIA/SERUH VASIES		0.1	LITERS L CELLS/L FLASK G@/LITER
113	BIOSYNTHESIS BIOFEACTOR PREPARATION (STIPPED TANK REACTOR)	PEACTOR FEED YOU'VE SPINKER/PEACTOR RATIO CCAPRIER DENSITY NUMBER OF PES WASTES NUMBER OF MEDIA VASTES NO. OF MEDIA/SERUN WASTES		500 8.3 · S 1 2	LITERS Ge/LITER
	BIOSYNIHESIS BIOFEACTOR PREPARATION (FLUIDIZED BED REACTOR)	PEACTOR FEED YOU'FE UCAPRIER DENSITY NUMBER OF PRS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERRI WASHES SERUH CONTENT			LITERS Gas/L
115	INITIAL COUPLING	FLASK FEED VOLUME VESSEL/FLASK RATIO UCAPRIER DENSITY NUMBER OF PBS VASIES NUMBER OF MEDIA VASIES HO. OF HEDIA/SERUN VASIES		0.1 5 2 1	LTIERS L CELLS/L FLASX Ge/LITER FBS
TIS	ADDITIONAL COUPLING	REACTOR FEED VOLUME SPINNER/REACTOR RATIO UCAPRIERI DENSITY MURGER OF PRS VASSES NUMBER OF MEDIA VASSES NO. OF MEDIA/SERIM VASSES		8.3	LITERS Ga/LITER
TI	PEPTIDE CLEAVAGE	REACTOR FEED VOLUME MUMBER OF PRS VASSES MUMBER OF MEDIA VASSES HO. OF MEDIA/SERUH VASSES SERUH CONTENT		2 2 2	LITERS FETAL BOYINE SERVA
	LISZAE LHARINE	CRUDE PRODUCT YEILD ENVIRONMENTAL TEMPERATURE THAY DURATION		25 25	GO CHUDE PROD./Kg TISSUE
	HOLTAZIHGBOHOH	CRUDE PRODUCT YEILD LIQUID/SOLID RATIO HUMOGENIZATION TEMP. HUMOGENIZER TYPE ENERGY IMPUT DURATION		10 4 RS 200	Ga CRUDE PROD./Kg TISSUE L SOLUTION/KG TISSUE C HP/100L/HR HOURS
1150	ICTANTA IUMATUR	1			

FIG. 158

	SROUP 2	F16.	158	GROUP 3
PARAVETER	SOLN.		PARWETER	SOLN.
PBS YASIES HEXY NISCYTRI		200 HI 100 HI		
FEED RATE Days to confluence PBS Washes Trypson Wash		I FEED PER WESSEL 2 DAYS 2 DAYS 200 HI 100 HI	PER APPLIFICATION FACTOR	100%
SERUM CONTENT FEED RATE DAYS TO CONFLUENCE		2.0% FETAL BOVINE SE 1 FEED PER VESSEL 2 DAYS 2 DAYS	RUN AMPLIFICATION FACTOR Per	100%
SERIM CONTENT FRED RATE DAYS TO CONFLUENCE SERIA FREE MEDIA VASHES		2.0% FEIAL BOYINE SE 1 FEED PER YESSEL 2 DAYS 10 DAYS 2	FINE PRODUCT CONCENTRATION PER TOTAL PROTEIN CONCEN.	2500% Ng PROD/L 0.125 Ng TP/NJ
NUMBER OF REACTORS FEED RATE DAYS TO CONFLUENCE		1 1 FEED PER VESSEL 1 DAYS 10 DAYS	PRODUCT CONCENTRATION PER TOTAL PROTEIN CONCEN.	2500% Ng PROD/L 0.125 Ng TP/HI
SERUN CONTENT FEED RATE DAYS TO CONFLUENCE		2.0% FETAL BOYINE SE 1 FEED PER VESSEL 2 DAYS 2 DAYS	RUM APPLIFICATION FACTOR PER	100%
SERUM CONTENT FEED PATE DAYS TO COMPLUENCE SERUM FREE MEDIA WASHES		2.0% FETAL BOVINE SE 1 FEED PER VESSEL 2 DAYS 10 DAYS 2	PER TOTAL PROTEIN CONCENT.	2500% Ng PROD/L 0.125 Ng TP/MI
NUMBER OF REACTORS FEED RATE DAYS TO CONFLUENCE		1 FEED PER VESSEL 1 DAYS 10 DAYS	HARVEST VOLUME PRODUCT CONCENTRATION TOTAL PROTEIN CONCEN.	500% LITERS 25 Hg PROD/L 0.125 Hg TP/HI
CONTANINANT PROTEIN CONC.		100 Ga/L	TEXPERATURE REGULATION CIP SIP	Y
CONTANIDANT PROTEIN CONC.		100 Ga/L	TEPFERATURE REGULATION CIP SIP	YYY
	-		AMPLIFICATION FACTOR	100%

FTG 164

		FIG. 18	4	
			GROUP 1	
<u> </u>	UNIT OPERATION TYPE	PARAMETER	OLN.	
T21	PRODUCT Ppt BY SOLIDS	REAGENT CONCENTRATION	1	H
T22	PRODUCT Ppt BY LIQUIDS	REAGENT CONCENTRATION	í	H
123	CONTAINMENT PP4 BY SOLIDS	REAGENT Concentration	1	H
	CONTAINMENT Ppt BY LIQUIDS	REAGENT CONCENTRATION	1	
125	SOLIDS HARYEST Tangential flow Af	POROSITY AVERAGE FLUX RATE TOTAL THROUGHPUT FILTRATION TIME	11 40 4	LITERS/SF
T26	CONTINUOUS CENTRIFUGATION SOLIDS HARVEST	SYSTEM YOLD VOLUNE		LITERS
T27	CONTINUOUS CENTRIFUGATION SUPERIVATANT HARVEST	SYSTEM VOID VOLUME	6	LITERS
	DILUTION .	SYSTEM VOID VOLUME	6	LITERS
T29	BATCH CENTRIFUGATION SOLIDS HARYEST	SYSTEM VOID VOLUME	6	LITERS

		FIG. 1	68		
	2 ROUP 2			ROUP 3	
PARAMETER	SOLN.	•	PARAVETER	SOLH.	
Koas of Reagent/Liters product Teperature Adoltion tipe Adoltional hix tipe	0.5	Kg/L C Hours Hours	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TERPERATURE REGULATION CIP STP		95% 95% Y Y
LITERS REASONT/LITERS PRODUCT TEXPERATURE ADDITION TIME ADDITIONAL HIX TIME	0.5	C Hours Hours	SIEP RECOVERY OF PRODUCT SIEP RECOVERY OF T.P. TEXPERATURE REGULATION CIP SIP		95% 95% Y Y Y
Kg3s OF HEADENT/LITERS PRODUCT TEMPERATURE ADDITION TIPE ADDITIONAL MIX TIME	0.5	Kg/L C Hours Hours	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEXPERATURE REGULATION CIP STP		32.2 32.2 32.2 32.2 32.2 32.2 32.2 32.2
LITERS REAGENT/LITERS PRODUCT TEMPERATURE ADDITION TIME ADDITIONAL HIX TIME	0.5	L/L C Hours Hours	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		95% 95% Y Y
FLUSH PRIME CONCENTRATION FACTOR VASH RECENERATE STORE	2 10 0.5 1	LISF LISF FOLD LISF LISF LISF	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP STP		A A 32% 32%
RCF TIME VOLUME REDUCTION VASH VOLUME	10,000 60 30		SIEP RECOVERY OF PRODUCT SIEP RECOVERY OF J.P. IEPPERATURE REGULATION CIP SIP	- 1	95% 95% Y Y
RCF TIPE VOLUPE REDUCTION VASH YOURE	0.062	X 6 NINUTES YOL. REDUCTION X SYSTEM YOID VOLUME	SIEP RECOVERY OF PRODUCT SIEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	- 1	85% 0.3 Y Y
RCF TIHE YOLUFE REDUCTION WASH YOLUFE	15	X SAZIEH AOID AOITHE X Aof Georgion X e	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	1	55% 0.95 Y Y
RCF TIME	10.000 30	X 6 Hinutes	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P.		95% 0.95

Title: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown

47A ETC

	FIG. 17A							
		ALDIVETED.	ROUP 1					
$\vdash$	UNIT OPERATION TYPE	PARAMETER	SOLN.					
130	BATCH CENTRIFUGATION SUPERNATANT HARVEST	SYSTEM VOID VOLUME		6 LITERS				
T31	CELL DISPUPTION High Press. Hohogen.	PRODUCT TEMPERATURE UTILITY TEMPERATURE VOID VOLUME		8 C 2 C 5 Liters				
132	CELL DISPUPTION BEAD HILL	MUMBER OF PASSES BEAD SIZE YOID YOLUNE FLOW RATE		0.5 LPH				
133	CELL DISPUPTION CHEHICAL LYSIS	PEAGENT TEHPERATURE EXPOSURE TIME		0.5 H Nach 4 C 2 Hours				
134	MICROFILTRATION TANGENTIAL FLOW	POROSITY AVERAGE FLUX RATE TOTAL THROUGHPUT FILTRATION TIME		0.2 HICRON 50 L/SF/HR AT 40 PSIG AT 4 C 400 LITERS/SF 2 HR				
135	HICROFILTRATION DEAD END	POROSITY AYERAGE FLUX RATE TOTAL THROUGHPUT FILTRATION TIME		0.2 HICRON 50 L/SF/HR AT 40 PSIG AT 4 C 400 LITERS/SF 0.5 HR				
T36	ULTRAFILTRATION CONCENTRATION/DILUTION	POROSITY AVERAGE FLUX RATE CONCENTRATION TIME		60 K 1299A 3 L/SF/HR AT 40 PSIG AT 4 C 2 HR.				
13	ULTRAFILTRATION FLOW DIALYSIS	POROSITY AVERAGE FLUX RATE		GO K MATA 3 L/SF/AR AT 40 PSIG AT 4 C				

FIG. 17B						
	PROUP ?		GROUP 3			
PARAMETER	SOUN.	PARAMETER	SOLH.			
VOLUME REDUCTION VASH VOLUME	16 X VOL. REDUCTION 1.5 X SYSTEM VOID VOLU	CIP SIP	Y			
RCF TIME VOLUME REDUCTION WASH VOLUME	19000 X G 30 MINUTES - 16 X VOL. REDUCTION 1.5 X SYSTEM VOID VOLU	STEP RECOVERY OF PRODUCT STEP RECOVERY OF 1.P. TEMPERATURE REGULATION CIP SIP	95% 0.35 Y Y Y			
NUMBER OF PASSES PRESSURE PLOW RATE TEMPERATURE INCREASE	6 TIMES 12,000 PSI 5 LPM 1.8 DEGREES C/1,000 PS	CIP CIP	SOOX YOID VOLUHES 95X 95X Y Y Y			
		STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CTP SIP	95% Y Y Y			
LITERS REAGENT/Gm PRODUCT TITRATION	0.4 L/Gm 0 HI/LITER	SIEP RECOVERY OF PRODUCT SIEP RECOVERY OF I.P. TEMPERATURE RESULATION CIP SIP	95X Y Y Y			
FLUSH PRIME VASH SOLIOS REGENERATE STORE	2.00 L/SF 2.00 L/SF 0.50 L/SF 0.30% OF PRODUCT SOLUTIO 1.00 L/SF 2.00 L/SF	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. IN TEMPERATURE REGULATION CIP STP	953 953 Y Y			
FLUSH PRINE VASH SOLIDS PEGENERATE STORE	0 L/SF 0 L/SF 0.5 L/SF 0.003 OF PRODUCT SOLUTIO 1 L/SF 2 L/SF	STEP RECOVERY OF PRODUCT STEP RECOVERY OF 1.P. IN TEMPERATURE REGULATION CIP STP	95% 0.95 N N N			
FLUSH PRIME VASH DILUTE CONCENTRATE SOLIDS FEGENERATE	2.00 L/SF 2.00 L/SF 0.50 L/SF 10.0 FOLD 0.30% OF PRODUCT SOLUTION 1.00 L/SF	STORE STEP RECOVERY OF PRODUCT STEP RECOVERY OF 1.P. TEMPERATURE RESULATION CIP SIP	2.00 L/SF 95% 95% Y Y Y			
FLUSH PRIME DIALYSIS BUFFER VASH	2 L/SF 2.00 L/SF 5.0 x feed stream vol 0.50 L/SF	STORE STEP RECOVERY OF PRODUCT UNE STEP RECOVERY OF T.P. TEMPERATURE REGULATION	200% L/SF 95% 95% Y			

FIG. 18A

_		F16. 10		
	11177 AREA TOAL TIME			ROUP 1
	UNIT OPERATION TYPE	PARAVETER	SOLH.	
		DIALYSIS TIME		2 HR
T38	PROD. ADS. CHROMATOGRAPHY HPLC	COLUMN CAPACITY COLUMN OVERSIZE FACTOR COLUMN ASPECT RATIO MAX. LINEAR VELOCITY		10 Mg PROO./MI OF PACKING 1.5 FOLD 0.37 H/O 100 Cm/HR AT 45 PSIG AND 4 C
139	PROO. AOS. CHROMATOGRAPHY MPLC	COLURN CAPACITY COLURN CYPERSIZE FACTOR COLURN ASPECT PATIO NAX. LINEAR VELOCITY		10 Mg PROD./MI OF PACKING 1.5 FOLD 0.37 H/D 100 Cm/Hr at 45 PSIG AND 4 C
T40	PROD. ADS. CHROMATOGRAPHY LPLC	COLUMN CAPACITY COLUMN OVERSIZE FACTOR COLUMN ASPECT RATIO MAX. LINEAR VELOCITY		10 Mg PROD./HI OF PACKING 1.5 FOLD 0.37 H/D 100 Cm/HR AT 45 PSIG AND 4 C
T41	CONT. ADS. CHROMATOGRAPHY HPLC	COLUMN CAPACITY COLUMN OYERSIZE FACTOR COLUMN ASPECT RATIO MAX. LINEAR YELOCITY		30 Ng CONT./MI OF PACKING 1.5 FOLD 0.37 H/D 100 Cm/HR AT 45 PSIG AND 4 C
T42	CONT. ADS. CHROMATOGRAPHY MPLC	COLUMN CAPACITY COLUMN OVERSIZE FACTOR COLUMN ASPECT RATTO NAX. LINEAR YELOCITY		10 Mg CONY./MI OF PACKING 1.5 FOLD 0.37 H/D 100 Cm/HR AI 45 PSIG AND 400% C
	CONT. ADS. CHROMATOGRAPHY LPLC	COLUMN OVERSIZE FACTOR COLUMN ASPECT RATIO NAX. LINEAR VELOCITY		10 Mg CONT./HI OF PACKING 1.5 FOLD 0.37 H/D 100 Cm/HR AT 45 PSIG AND 4 C
144	SIZE EXCL. CHROMATOGRAPHY HPLC	LOAD CAPACITY LENGTH MAX. LINEAR VELOCITY VOID VOLUNE		S% OF TOTAL COLUMN VOLUME 100 Cm 100 Ca/HR AT 45 PSIG AND 4 C - 25% COLUMN VOLUME
145	SIZE EXCL. CHRICHATOGRAPHY MPLC	LOAD CAPACITY LENGTH MAX. LINEAR VELOCITY YOUD YOURE		5% OF TOTAL COLUMN VOLUME 100 Cm 100 Cm/Hr at 45 PSIG AND 4 C 25% COLUMN VOLUME

		8B	
6	ROUP ?	6	300 3
PARAMETER	SOLN.	PARAMETER	SOLH.
SOLIDS RESENERATE	0.30% OF PRODUCT SOLUTION 1.00 L/SF	CIP SIP	Υ. Υ
COLUMN EQUILIBRATION COLUMN WASH COLUMN ELUTE A COLUMN ELUTE B COLUMN REGENERATE COLUMN STORE	5 COTAN AOTHES 1 COTAN AOTHES 2 COTAN AOTHES 3 COTAN AOTHES 2 COTAN AOTHES 2 COTAN AOTHES	PROD. ELUTION YOUNE STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	80% 95% 95% N Y Y
COLUMN EQUIL IBRATION COLUMN MASH COLUMN ELUTE A COLUMN ELUTE B COLUMN REGENERATE COLUMN STORE	S COLUM AOTINES  1 COLUM AOTINES  2 COLUM AOTINES  3 COLUM AOTINES  4 COLUM AOTINES	PROD. ELUTION YOLUNE STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	A A BOX 82X 80X
COLUMN EQUIL IBRATION COLUMN MASH COLUMN ELUTE A COLUMN ELUTE B COLUMN FEEDWERATE COLUMN STORE	S COTINA ADTINES  1 COTINA ADTINES  5 COTINA ADTINES  3 COTINA ADTINES  2 COTINA ADTINES  2 COTINA ADTINES	PROD. ELUTION VOLUME STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP STP	A A B B2x 82x 82x
COLUMN COUIL IBRATION COLUMN YASH COLUMN ELVITE A COLUMN ELVITE B COLUMN REGENERATE COLUMN STORE	S COLUMN YOLUMES COLUMN YOLUMES COLUMN YOLUMES COLUMN YOLUMES COLUMN YOLUMES	PROD. ELUTION YOLUNE STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP STP	42% 95% 95% 95 9 1 1 1
COLUMN EQUIL IBRATION COLUMN WASH COLUMN ELUTE A COLUMN ELUTE B COLUMN REGENERATE COLUMN STORE	S COLUMN YOUMES  1 COLUMN YOUMES  2 COLUMN YOUMES  5 COLUMN YOUMES	PROO. ELUTION VOLUME- SIEP RECOVERY OF PRODUCT SIEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	42% 953 953 953 N Y Y
COLUMN ECUTLIBRATION COLUMN WASH COLUMN ELUTE A COLUMN ELUTE B COLUMN FEGENERATE COLUMN STORE	S COLUMN VOLUMES 3 COLUMN VOLUMES 4 COLUMN VOLUMES 1 COLUMN VOLUMES 2 COLUMN VOLUMES	PROO. ELUTION VOLUME STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP STP	42% COLUMNS VOLUMES 95% 95% N N Y
COLUMN EQUIL IBRATION COLUMN YASH COLUMN PEGENERATE COLUMN STORE	4 COLUMN VOLUMES 1 COLUMN VOLUMES 2 COLUMN VOLUMES	PROO. ELUTION VOLUME STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CTP STP	42% COLUMNS VOLUMES 95% 95% N Y Y
COLUM EQUILIBRATION COLUMN WASH COLUMN REGENERATE COLUMN STORE	S COLUMN AOTINES T COTINN AOTINES T COTINN AOTINES	PROD. ELUTION VOLUME STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	42% COLUMNS VOLUMES 95% 95% N Y Y

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Inventor: Peter G. Brown

FIG. 19A

_		F1G. 13			
1				SROUP 1	
_	UNIT OPERATION TYPE	PARAMETER	SOLN.		
T46	SIZE EXCL. CHRONATOGRAPHY LPLC	LOAD CAPACITY LENSTH HAX. LINEAR YELOCITY VOID VOLUME		100 100 45 4	OF TOTAL COLUMN VOLUME CM CM/HR AT PSIG AND C COLUMN VOLUME
147	DILUTION	DILUTION FACTOR			LITERS/LITER
	RESOLUBILIZATION	REGEANT/PRODUCT RATIO  DISSOLUTION TINE ADDITIONAL MIX TIME		0.50 0.50	L/Kg PRODUCT Hours Hours
T49	ENZYMATIC HODIFICTATION	ENZYME TO PRODUCT RATIO ENZYME CONCENTRATION REACTION TEMP. REACTION DURATION		2 37	LITERS OF ENZYME STOCK PER LITER OF START. PROC. VOL. Mg/MI Despees C Minutes
<b>T50</b>	LYOPHILIZATION .	PRODUCT CAPACTTY/LOAD PRODUCT UNIT SIZE			UNITS Grans/unit
<b>T51</b>	HEAT EXCHANGE	PROCESS INITIAL TEMP PROCESS FINAL TEMP UTILITY INITIAL TEMP UTILITY FINAL TEMP PROCESS SPECIFIC HEAT DESIGN TYPE (P.I.C)		39.2 34 5	DEGREES C Degrees C Degrees C Degrees C K BTU/AR
152	STORAGE			•	
	FERMENTATION SEED	SCALE UP RATIO FERMENTOR WORKING VOLUME ANTIFOAN A ANTIFOAN 8 BASE ACID		91155	FOLD LITERS NI/L NI/L NI/L MI/L
154	INITIAL SEEDING	FLASK FEED VOLUME SPINNER SPLIT RATIO		12 4	LITERS

FIG. 19B

	2 ROUP	F16. I	JD 0	POUP 3	
PARAMETER	SOLN.		PARWETER	SOLH.	
COLUM EQUILIBRATION COLUM VASH COLUM REGENERATE COLUM STORE	Juli.	4 COLUMN VOLUMES 1 COLUMN VOLUMES 2 COLUMN VOLUMES	PROD. ELUTION VOLUME STEP RECOVERT OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		42X COLUMN YOLUMES 95X 95X N Y
DILUTION TIPE ADDITIONAL MIX TIPE		0.5 HOURS 1 HOURS	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP STP		95% 95% Y Y Y
REGEART 1 Concentration		MATER DIST.	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. Temperature regulation CIP STP		95% 95% Y Y
TITRATION SOLUTION-1 TITRATION SOLUTION-2 NEUTRALIZATION		0.057 L/L PROCESS 0.02 L/L PROCESS 0.57 L/L PROCESS	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REBULATION CIP SIP		95% 95% Y Y
LYOPHILIZATION TIME PRODUCT NEIGHT REDUCTION		18 HOURS 0.95	STEP RECOVERY OF T.P.  CIP SIP		95% 95% Y Y
EXPOSURE TIME		1 HOURS	SIEP RECOVERY OF PRODUCT SIEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		100% 100% Y Y Y
			STEP RECOVERY OF PRODUC STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP STP		95% 95% Y Y Y
CHOYTH TEMPERATURE AGITATION SPAREE RATE BACK PRESSURE TOTAL DURATION		37 HOURS 1 HP/100L 1.5 WM 5 PSIG 21 HPS	CIP		12 - Y
SERUM CONTENT FEED RATE		2% FBS 1 FEED PER VESSEL PER	AMPLIFICATION FACTOR		1

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FIG. 20A

			6	AOP 1
	UNIT OPERATION TYPE	PARAMETER	SOUN.	
		UCARRIER DENSITY NUMBER OF PBS VASHES NUMBER OF HEDIA VASHES NO. OF MEDIA/SERUN VASHES		5 Ga/LITER 2 · 1 2 FBS
T55	CULTURE VESSEL SPLIT	PLASK FEED VOLUME SPINNER SPLIT RATIO UCARRIER DENSITY NUMBER OF PRS VASSES NUMBER OF MEDIA VASSES NO. OF MEDIA/SERIM VASSES		12 LITERS  4 SEMILITER 2 1 2 FBS
156	CULTURE FLASK SPLIT			
	STIPRED TANK REACTOR			
TS8	FLUIDIZED BED REACTOR	PROCESS INITIAL TEMP PROCESS FINAL TEMP UTILLITY INITIAL TEMP UTILLITY FINAL TEMP PROCESS SPECIFIC HEAT DESIGN TYPE (P.T.C)		37 DEGREES C 4 DEGREES C 2 DEGREES C 5 DEGREES C 12 K BTV/HR
155	LIQUID/LIQUID EXTRACTION	LIQUID/LIQUID RATIO EXTRACTION TEMPERATURE ADDITION DURATION ADDITIONAL MIX. DURATION MIX ENERGY		1 L EXTRACTION/L PRODUCT 4 C 0.5 Hours 4 Hours 0.3 HP/100L
TE	SOLID/LIQUID EXTRACTION	LIQUID/LIQUID RATIO EXTRACTION TEMPERATURE DURATION NIX ENERGY		1 L EXTRACTION/L PRODUCT 4 C 4 C 4 HOURS 0.3 HP/100 L

FIG. 20B

	GROUP 2			<b>OUP 3</b>	
PARAMETER	SOLN.		PARAMETER	SOLH.	
DAYS TO CONFLUENCE	5 D				
SERUM CONTENT FEED RATE DAYS TO CONFLUENCE	2% F	HED PER VESSEL PER	AMPLIFICATION FACTOR		i
			STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P.		0.95 95X Y
EXPOSURE TIME	50% H	DURS	STP STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP		0.95 100%
PHASE SEPARATION TIME PRODUCT PHASE (TOP/BOTTON) HARVEST TIME	1600% 1 TOP 0.5 1		SIP PECOVERY OF PRODUCT SIEP PECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		0.9 50%
PHASE SEPARATION TIME PRODUCT PHASE (TOP/BOTTON) HARVEST TIME	1600X TOP 0.5	HOURS HOURS	SIEP RECOVERY OF PRODUCT SIEP RECOVERY OF T.P. IEMPERATURE REGULATION CIP SIP		0.9 50% Y Y Y

			<u>R</u>	Process Design Cycles	ign (	Sydes						
90n				Unit Op		Cnit	Jnit Op Cluster	. 16			Batch	
Seq.	Seq.	Unit Operation Type		Offset (Hrs)		UnOp Start	UnOp End	Offset (Hrs)		UnOp Start	UnOp End	Offset (Hrs)
-	89	STR-Suspension Production	γ-	0	_			0	-			0
2	74	Harvest/Feed-Suspension Production	က	24				0	20	8	4	72
က	8	Tangential Flow-Clarification	_	0			_	0	20	7	4	72
4	47	Dilution	-	0	Ψ-			0	20	7	4	22
သ	66	End										
2102 2104	<u>\$</u>	2106		2108 2110 2112 2114			2116	2118 2120 2122			2124	2126

			Pol	Process Design Cycles	ign (	Sycles						
9				Unit Op		Cult	Unit Op Cluster	50			Batch	
S & S	Code	Unit Operation Type		Offset (Hrs)		UnOp Start	UnOp	Offset (Hrs)		UnOp Start	UnOp	Offset (Hrs)
10301	87	Pool			_				-			
10302	51	Heat Exchange	_		_				-			
10303	56	Cont. Centrifugation - Solids Harvest	_		-				-			
10304	84	Resolubilization	-		-				-			
10305	61	Inlet Heat Exchange	-		ო	Ŋ	7		-			
10306	31	High Pressure Homogenization	_		က	ß	7	တ	_			
10307	51	Outlet Heat Exchange			ო	Ŋ	2	တ				
10308	29	Batch Centrifugation - Solids Harvest	<b>~</b>		_				_			
10309	29	Dilution - 18 Wash	-		7	တ	9		-			•
10310	58	Batch Centrifugation - Solids Harvest	_		7	თ	10		-			
10311	63	Storage	-		-				_			
10312	66	End	-		<del>-</del>				_			
2202 2204	<b>A</b>	2208/ 2208/		2210/ 2212/ 2214	2 2		2216	2218 2220	_	2222	2224	2226
				FIG. 22	2							

Title: The Use of Sub (Partial) Cycles, ...
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				· · · · · · · · · · · · · · · · · · ·	···	
	OPERATION		CALC	CULATIONS		
1111 T76	NAUTI-STAGE POOL	LINK				
	SET UP	SOURCE				
	NPUI 1 NPUI 2	PE-0102e	20272.98 UTERS @ 0 UTERS @	104.00 HOURS, TRANSFER IN 0.00 HOURS, TRANSFER IN	O.O HOURS= O.O HOURS=	0.0 LP
	NPUT 3		O LITERS 0	0.00 HOURS, TRANSFER IN	OLD HOURS=	0.0 LP 0.0 LP
	NPUT 4 NPUT 5		O LITES <b>e</b> O LITES <b>e</b>	0.00 Hours, Iransfer in 0.00 Hours, Iransfer in	0.0 HOURS= 0.0 Hours=	0.0 LP
	NPUI 6	j	O LITERS O	0.00 Hours, Transfer in	0.0 HOURS=	0.0 LP1 0.0 LP1
	POOL INPUTS SUB TOTAL		20272.98 LITERS IN	0.00 HOURS, TRANSFER IN 104.00 TOTAL TRANSFER	0.0 HOURS=	0.0 191
	SUD TUTHE			INTO THIS TRANSFER	0 HOURS	LPM NESC
2.1.1.1 51	OUTLET HEAT EXCHANGE					
	SET UP Transfer	20,273.0 t EH	2.50 HRS =	135.2 LPM		
	WASH	20,273.9 C th	∠JU NK3 =	IND.Z (CM		
	ZB, CB,					
	CLEAN UP					
	SUB TOTAL			135.2		
3.1.1.1 26	COMT. CERT/SOLIDS					
	SII UP			£ 7 . m.		
	CENTRIFUGATION Wash	20,273.0 L IN 30.0 L IN	5.00 HRS = 0.01 HRS =	56.3 LPM 56.3 LPM		
	CIP SEP					
	CLEAN UP					
	SUB TOTAL			56.3 LPN		
4.1.1.1 48	RESOLUBILIZATION				· · · · · · · · · · · · · · · · · · ·	
	STI UP	54755 1 81	30.0000	20.0 (0)		
	DILUTION NO	6,476.0 L IN	3.0 HOURS 0.0 Hours	38.0 LPM		
	CP SP					
	CLEAN UP					
	SUB 10TAL			36.0		
5.1.1.1 61	INLET HEAT EXCHANGE					<del>.</del>
	ST UP					
	TRANSFER Wash	8,634.7 L EN 0.0 L EN	2.5 HRS = 0.0 HRS =	57.56 LPN 0.0 LPN		
	ر	WA CRI		~		
	2302		2	2304		

FIG.23A-1

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URATION	(HRS)		REL 11	E SCALE	(HRS)	ABS. H	OURS	A8S. D	ays_	SIARI		FINISH	
CALC	ιœ	ADL	PREP	EXEC.	COMPL	START	END	START	010	CATE	THE	DATE	TM
0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0	22 0.0 22 0.0 22 0.0 22 0.0 23 0.0 23 0.0 23 0.0	104.0	104.0		1649 1649 1649 1649 1649 1649 1649 1649	104.0 104.0 0.0 0.0 0.0 0.0	77888888888888888888888888888888888888	433 433 688 688 688 688 688 688 688 688 688 6	01/ <b>08/99</b> 01/08/99	06:00 AM MA 00:30	01/08/99 01/08/99	08:00 A 08:00 A
00 00 00 00	0.0 0.0 0.0	0.0 HRS 28H 0.0 28H 0.0 28H 0.0		104.0 104.0		0.0 0.0 104.0	20 20 104.0 20	472 000 000	68 69 43 43	01/08/99 01/08/99	05:00 AM	01/08/99 01/08/99	A 00:80 A 00:80
										HRS/CY	0.0		
1.0 2.50 0.63 0.0 0.0 2.0	0.0 0.0 0.0 0.0 0.0	1.0 HRS 2.5 HRS 0.5 HRS 0.0 HRS 0.0 HRS 2.0 HRS	104.0	105.5 107.1	107.1 107.1 109.1	103.9 104.0 106.3 107.1 107.1 107.1	104.0 105.5 107.1 107.1 107.1 109.1	4.28 4.33 4.44 4.46 4.46 4.46	4.33 4.44 4.46 4.46 4.46 4.55	01/08/99 01/08/99 01/08/99 01/08/99	07:00 AM 08:00 AM 10:30 AM 11:07 AM 11:07 AM 11:07 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	08:00 A 10:30 A 11:07 A 11:07 A 11:07 P
5.1		5.1 HRS		105.5			*	32.5		01/08/99 HRS/CY	07:00 AM 5.1	01/08/99	01:07 P
1.0 6.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0	28H 0.1 28H 0.0 28H 0.0 28H 0.0 28H 0.0 28H 0.0	105.6	1125 1125	1125 1125 1125	105.6 106.5 112.5 112.5 112.5 112.5	106.5 112.5 112.5 112.5 112.5 112.5	4.00 4.64 4.68 4.68 4.68 4.68	4.44 4.64 4.68 4.68 4.68 4.68	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	04:30 PM	01/08/99 01/08/99 01/08/99	10:30 A 04:30 P 04:30 P 04:30 P 04:30 P
7.0		7.0 HRS		112.5			112.5			01/08/99 HRS/CY	09:30 AM 3.0	01/08/99	04:30 P
1.0 3.00 0.00 0.0 0.00	0.0 0.0 0.0 0.0 0.0 0.0	1.0 H/S 3.0 H/S 0.0 H/S 0.0 H/S 0.0 H/S 1.0 H/S	112.6	115.5 115.5	115.5 115.5 116.5	111.0 112.5 115.5 115.5 115.5 115.5	112.0 115.5 115.5 115.5 115.5 118.5	4.85 4.88 4.81 4.81 4.81	4.68 4.81 4.81 4.81 4.81 4.85	01/08/99 01/08/99 01/08/99 01/08/99	07:30 PM 07:30 PM 07:30 PM 07:30 PM	01/08/99	04:30 P 07:30 P 07:30 P 07:30 P 07:30 P 08:30 P
5.00		5.00 HRS	-	115.5						01/08/99 BSS/CY	03:30 PM 5.0	01/08/99	08:30 P
1.0 250 0.00	0.0	1.0 HRS 2.5 HRS 0.0 HRS	115.5	118.0 118.0	,	114.5 115.5 118.0	115.5 118.0 118.0	4.81	4.92	01/08/99	06:30 PM 07:30 PM 10:00 PM	01/08/99	07:30 F 10:00 F 10:00 F
) 306	1	2310	1	2314	. )	2318	3	23	22	2324	2326	2328	233

Title: The Use of Sub (Partial) Cycles, ...
Inventor: Peter G. Brown

	OPERATION			CA	LCULATIONS	
	CIP					
	SIP CLEAN UP					
	SUB TOW				57.6	
,						
5.1.1.1 31	HOMMOGENIZATION					
	SET UP	70747 4 NI	A C 1700		77.4 10H	
	LYCIS WASH	3834.7 L IN 0.0 L IN	2.5 HPS 0.0 HPS		57.6 LPM 0.0 LPM	
	CIP	<b>V.</b> C			V.4 B =	
	SIP CLEAN UP					
	SUB TOTAL			5	7.564344	<del></del>
7.1.1.1 51	OUTLET HEAT EXCHANGE					
	SET UP					
	IRANSTER Wash	3543.7 L IN 0.0 L IN	2.5 HRS 0.0 HRS	=	57.58 LPM 0.0 LPM	
	OP I		0.5 7.00		0.0 D m	
	SIP Clean up					
	SUB TOTAL				57.56	······································
5.1.2.1 61	INLET HEAT EXCHANCE					
	SET UP Transfer	ACT 2 2 4 40	8.6 1100		53.58 thu	
	WASH	8634.7 L EN 0.0 L EN	2.5 HRS 0.0 HRS		57.55 LPM 0.0 LPM	
	CIP	5.5 E 4.1				
	SIP CLEAN UP					
•	SUB TOTAL					
6.1.21 31	HOMMOCENIZATION					
	SET UP	6774.7 1 111	0.5 100		53.5 10v	
	DILUTION NO	6834.7 L IN 0.0 L IN	2.5 HRS 0.0 HRS	=	57.6 1PM 0.0 1PM	
	QP .	2				
	SP CLEAN UP					
	SUB TOTAL				57.56	<del></del>

FIG.23B-1

Title: The Use of Sub (Partial) Cycles, ...
Inventor: Peter G. Brown

DURATION	(HRS)		REL III	E SCALE	(HRS)	ABS. H	DURS	A85. D	AYS	START		FINISH	
OLC.	roc	AOL	PREP	EXEC.	COMPL	START	END	START	DAD	DATE	IME	DATE	TM
00	0.0 0.0	0.0 HRS 0.0 HRS			118.0 118.0	118.0 118.0	118.0 118.0	4.92	4.92 4.92	01/08/99 01/08/99	10:00 PM 10:00 PM	01/08/99 01/08/99	10:00 P
0.0 2.5	0.0	0.0 HRS 2.5 HRS		116.0	118.0	118.0	118.0	4.92	492	01/08/99 01/08/99 HRS/CT DX	10:00 PM 06:30 PM 3.5	01/08/99	10:00 F
1.0 2.5 0.00 0.0 0.0	0.0 0.0 0.0 0.0 0.0	1.0 HS 2.5 HS 0.0 HS 0.0 HS 0.0 HS	118.0	120.5 120.5	120.5 120.5 120.5	117.0 118.0 120.5 120.5 120.5 120.5	118.0 120.5 120.5 120.5 120.5 120.5	88 28 28 88 28 28 88 28 28	######################################	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	08:00 AM 10:00 PM 12:30 AM 12:30 AM 12:30 AM	01/08/99 01/08/99 01/08/99	10:00 F 12:30 / 12:30 / 12:30 / 12:30 /
3.5		3.5 HRS		120.5			120.5			01/08/99 HRS/CY DX	09:00 PM 3.5	01/08/99	12:30 /
1.0 2.50 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0	1.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS	120.5	123.0 123.0	123.0 123.0 123.0	118.5 120.5 123.0 123.0 123.0 123.0	120.0 123.0 123.0 123.0 123.0 123.0	488 502 513 513 513 513	5.13 5.13 5.13 5.13	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	11:30 PM 12:30 AM 03:00 AM 03:00 AM 03:00 AM 03:00 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	12:30 / 03:00 / 03:00 / 03:00 / 03:00 /
2.5		2.5 HRS		123.0						01/08/99 HBS/CT	11:30 PW 3.5	01/08/99	03:00 /
0.0 2.50 0.00 0.0 0.0	0.0 0.0 0.0 0.0 0.0	0.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS	123.0	125.5 125.5	125.5 125.5 125.5	1230 1230 1255 1255 1255 1255	123.0 125.5 125.5 125.5 125.5 125.5 125.5	513 513 523 523 523 523 523	\$.13 5.23 5.23 5.23 5.23 5.23		03:00 AM 03:00 AM 05:30 AM 05:30 AM 05:30 AM		03:00 / 05:30 / 05:30 / 05:30 / 05:30 /
2.5		2.5 HRS		125.5 Q1F895						01/08/99 HRS/CY OK	03:00 AM 2.5	01/08/99	05:30 /
1.0 2.5 0.00 0.0 0.0	0.0 0.0 0.0 0.0 0.0	0.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS	123.0	125.5 125.5	125.5 125.5 125.5	123.0 123.0 125.5 125.5 125.5 125.5	123.0 125.5 125.5 125.5 125.5 125.5	513 513 523 523 523 523	5.13 5.23 5.23 5.23 5.23 5.23	01/08/99	03:00 AM 03:00 AM 05:30 AM 05:30 AM 05:30 AM 05:30 AM	01/08/99	03:00 / 05:30 / 05:30 / 05:30 / 05:30 /
25		2.5 HRS		125.5			125.5			01/08/99 HRS/CY	03:00 AN 2.5	01/08/99	05:30

FIG.23B-2

		<del></del>	<del></del>		
<del></del>	OPERATION		(	CALCULATORS	
	SET UP TRANSTER WASH CIP SP CLEAN UP SUB TOTAL	8543.7 L IN 0.0 L IN	25 HPS = 0.0 HPS =	57.56 LPM 0.0 LPM	
51.3.1 61	Inlet heat exchange set up transfer wash cip sip clean up sub total	8634.7 L BY 9.0 L BN	2.5 RRS = 0.0 RRS =	57.58 LPU 57.6 LPU	
6.1.3.1 31	HOMMOGENIZATION SET UP LYCS WASH CIP SIP CLEAN UP SUB TOTAL	8634.7 L IN 9.0 L IN	25 HRS = 0.0 HRS =	57.6 LPM 57.6 LPM	
2.1.3.1 51	OUTLET HEAT EXCHANCE SET UP TRANSFER WASH CIP SP CLEAN UP	8643.7 L IN 9.0 L IN	2.5 HRS = 0.0 HRS =	57.56 LPM 57.50 LPM 57.6 LPM	

FIG.23C-1

Title: The Use of Sub (Partial) Cycles, ...
Inventor: Peter G. Brown

DURATION	(HRS)		REL TA	e scale	(HRS)	ABS. H	OURS	A85. O	AYS	START		FINESH	
CALC	τοc	ADJ.	PREP	DEC.	COMPL	START	END	START	END	DATE	THE	DATE	
250 250 200 00 00 00	0.0 0.0 0.0 0.0 0.0	0.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS	123.0	125.5 125.5	185 185 185	133 133 133 133 133 133 133	1210 1255 1255 1255 1255 1255	5.13 5.13 5.23 5.23 5.23 5.23	5.13 5.23 5.23 5.23 5.23 5.23	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	03:00 AM 03:00 AM 03:00 AM 03:00 AM 03:00 AM 03:00 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	03:00 05:30 05:30 05:30 05:30
2.5		2.5 HRS		125.5						01/08/99 HRS/CY OK		01/08/99	653
0.0 2.50 0.0 0.0 0.0 0.0	0.0	0.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS	125.5	128.0 128.0	128.0 128.0 128.0	125.5 125.5 128.0 128.0 128.0 128.0	125.5 128.0 128.0 128.0 128.0 128.0	523 533 533 533 533	523 533 533 533 533 533	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	05:30 AM 05:30 AM 08:00 AM 08:01 AM 08:01 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	05:30 08:00 08:01 08:01 08:01
2.5		2.5 HRS		128.0						01/08/99 HRS/CY OK	05:30 Au 2.5		08:0
0.0 2.5 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0	25 00 25 00 25 00 25 00 25 00 25 00 25 00	125.5	128.0 128.0	128.0 128.0 128.0	125.5 125.5 128.0 128.0 128.0 128.0 128.0	125.5 128.0 128.0 128.0 128.0 128.0	323333	533 533 533 533	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	05:30 AM 05:30 AM 08:00 AM 08:01 AM 08:01 AM 08:01 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	05:30 08:00 08:01 08:01 08:01 08:01
2.5		2.5 HRS		128.0			128.0			01/08/99 HRS/CY " OK	05:30 AM 2.5	01/08/99	10:80
0.0 2.50 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0	668878 333333	125.5	128.0 128.0	128.0 128.0 128.0	125.5 125.5 128.0 128.0 128.0 128.0	125.5 128.0 128.0 128.0 128.0 128.0	523 523 533 533 533	5,33	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	05:30 AM 05:30 AM 08:01 AM 08:01 AM 08:01 AM 08:01 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	05:20 10:30 10:30 10:30 10:30

FIG.23C-2

Title: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown

	FIRST SHIF	I			ZECONO SHIT			
	START	07:00 AM	FINISH	03:00 PM	START	03:00 PM	FIXISH	11:00 Pt
OPERATIO	IN DATE	TIME	DATE	TME	DATE	TIME	DATE	TM
SET UP SET UP SPUT 1 SPUT 2 SPUT 3 SPUT 4 SPUT 5 SPUT 6 SPUT 6	01/08/99		01/08/99	MA 00:80 MA 00:80				
POOL IMPUTS SUB TOTAL	01/08/99	USTUU AM	01/08/99	08:00 AM				
2.1.1.1 51 OUTLET HEAT E SET UP TRANSFER WASH CP SIP CLEAN UP SUB TOTAL	C1/08/99 01/08/99 01/08/99 01/08/99 01/08/99	08:00 AM 10:30 AM 11:07 AM 11:07 AM	01/08/99 01/08/99 01/08/99	10:30 AM		-		
S.1.1.1 26 CONT. CERT/SC SCT UP CENTRIFUCATION WASH CIP SP CLEAN UP SUB TOTAL	01/08/99	09:30 AM 10:30 AM		10:30 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	04:30 PM 04:30 PM 04:30 PM 04:30 PM 04:30 PM	01/08/99 01/08/99	04:30 P
4.1.1.1 48 RESOLUBRIZATI SET UP CALUTION NO CIP SIP CLEAN UP SUB TOTAL	OH				01/08/99 01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	04:30 PM 07:30 PM 07:30 PM 07:30 PM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	07:30 P 07:30 P 07:30 P 07:30 P
5.1.1.1 61 INLET HEAT DI SET UP TRANSFER WASH	CHANCE				01/08/99 01/08/99 01/08/99	07:30 PM	01/08/99 01/08/99 01/08/99	10:00 F

FIG.23D-1

Title: The Use of Sub (Partial) Cycles, ...
Inventor: Peter G. Brown

DANG SHE			
	11:04 PM		04:07 AM
DATE	TIME	DATE	TIME
01/08/99	07:00 AM		
	1		
!			1

FIG.23D-2

Title: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown

	FIRST SHIF	ī			SECOND SHET			
	START	07:00 AM	FINISH	03:00 PM	START	01:00 PM	FINISH	11:00 PM
OPERATION_	DATE	THE	DATE	TIME	DATE	THE	DATE	TRAE
CP SP CLEAN UP SUB TOTAL					01/08/99 01/08/99 01/08/99	10:00 PM 10:00 PM 10:00 PM	01/08/99 01/08/99 01/08/99	10:00 PM 10:00 PM 10:00 PM
6.1.1.1 31 HOMBIOGENIZATION  SET UP LYCS WASH CP SP CLEAN UP SUB TOTAL					01/08/99 01/08/99	09:00 PM 10:00 PM	01/08/99	10:00 PM
7.1.1.1 51 OUTLET HEAT EXCHANGE SET UP TRANSFER TRASH CP SP CLEAN UP SUB TOTAL	GE .							
5.1.2.1 6) DILET HEAT EXCHANCE SET UP TRANSFER WASH CIP SIP CLEAN UP SUB TOTAL								
6.1.2.1 31 HONHOGENZATION  SET UP LYCS WASH CP SP CLEAN UP SUB TOTAL								
SUB TOTAL  7.1.2.1 51 OUTLET HEAT EXCHAN	CE							

Title: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown

TURON CLEE			
THERD SHE		Curen	00.00 411
START	11:00 PM		MA 00:80
DATE	TINE	DATE	THE
		01/08/99	12:30 AM
01/08/99	12:30 AM	01/08/99	12:30 AM
01/08/99	12:30 AM	01/08/99	12:30 AM
V1/00/33	12JU MI	01700733	
01/08/99	11:30 PM	01/08/99	12:30 AM
01/08/99	12:30 AM 03:00 AM	01/08/99	07-00 YM 07-00 YM
01/08/99	03:00 AM	01/08/99	03:00 AM
01/08/99 01/08/99	03:00 AM 03:00 AM	01/08/99 01/08/99	03:00 AM
			·
	i		
01/08/99 01/08/99	03:00 AM 03:00 AM	01/08/99 01/08/99	03:00 VM
01/08/99	05:30 AM	01/08/99	OSE NO AM
01/08/99 01/08/99	02:30 VM		05:30 AM 05:30 AM
01/08/99	MA 02:30	01/08/99	05:30 AM
01/00/00	01.00	01 (00 100	A3.A0 111
01/08/99 01/08/99	03:00 AM 03:00 AM	01/08/99	03:00 AM 05:30 AM
01/08/99 01/08/99	05:30 AM 05:30 AM	01/08/99	02-30 VA
01/08/99	05:30 AM 05:30 AM	01/08/99	05:30 AM 05:30 AM
7			
l	1		1

FIG.23E-2

Title: The Use of Sub (Partial) Cycles, ...
Inventor: Peter G. Brown

		FIRST SHIP				SECOND 3	₽Ĩ		
		START	07:00 AM	FEMISH	03:00 PM	START	03:00 PM	FINSH	11:00 PI
	OPERATION	DATE	TIME	DATE	TIME	DATE	THE	DATE	TM
	SET UP TRANSFER WASH CP SP CLEAN UP SUB TOTAL								
5.1.3.1 61	INLET HEAT EXCHANGE SET UP TRANSFER WASH CIP CLEAN UP SUB TOTAL	01/08/99 01/08/99 01/08/99 01/08/99	08:00 AM 08:01 AM 08:01 AM 08:01 AM	01/08/99 01/08/99	08:00 AM 08:01 AM 08:01 AM 08:01 AM 08:01 AM				
6.1.3.1 31	HOMOMOGENIZATION SET UP LYCIS WASH CIP SIP CLEAN UP SUB TOTAL	01/08/99 01/08/99 01/08/99 01/08/99	08:00 AM 08:01 AM 08:01 AM 08:01 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	08:00 AM 08:01 AM 08:01 AM 08:01 AM 08:01 AM				
7.1.3.1 51	CUTLET HEAT EXCHANCE SET UP TRANSFER WASH CP SEP CLEAN UP SUB TOTAL	01/08/99 01/08/99 01/08/99 01/08/99	08:01 AM 08:01 AM 08:01 AM 08:01 AM		08:01 AM 08:01 AM 08:01 AM 08:01 AM 08:01 AM				

FIG.23F-1

Docket No.: 3714.1000-000 Title: The Use of Sub (Partial) Cycles, ...

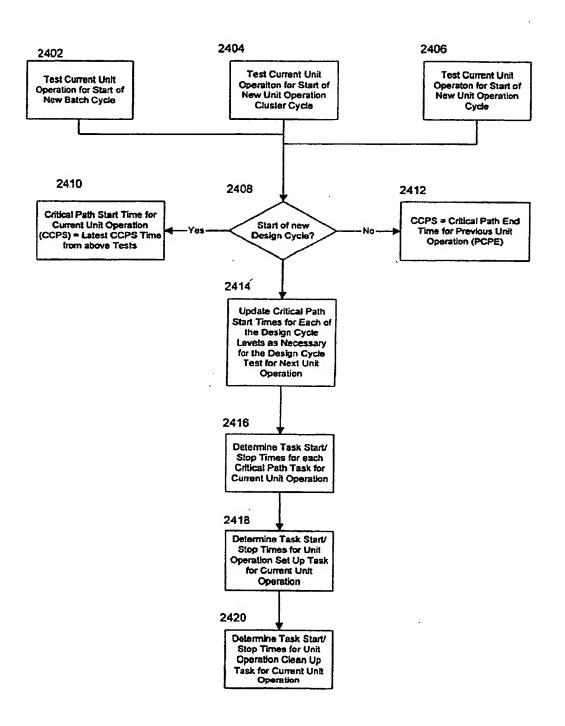
Peter G. Brown

THIRD SHIF	T		
START	11:00 PM	UMBH	05:30 AM
DATE	TIME	DATE	TIME
01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	03:00 AM 03:00 AM 05:30 AM 05:30 AM 05:30 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	03:00 AM 05:30 AM 05:30 AM 05:30 AM 05:30 AM
01/08/39 01/08/39	05:30 AM 05:30 AM	01/08/99	05:30 AM
01/08/99 01/08/99	05:30 AM 05:30 AM	01/08/99	05:30 AM
01/08/99 01/08/99	05:30 AM 05:30 AM	01/08/99	05:30 AM

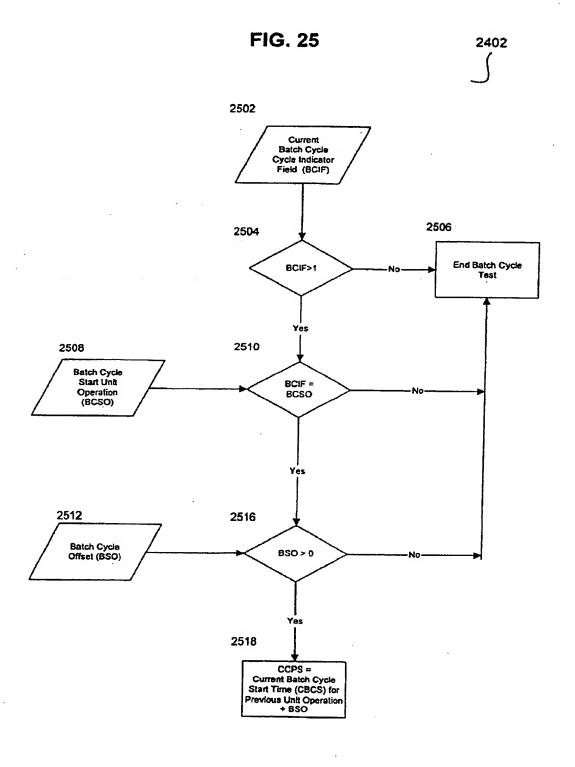
FIG.23F-2

Title: The Use of Sub (Partial) Cycles, ...

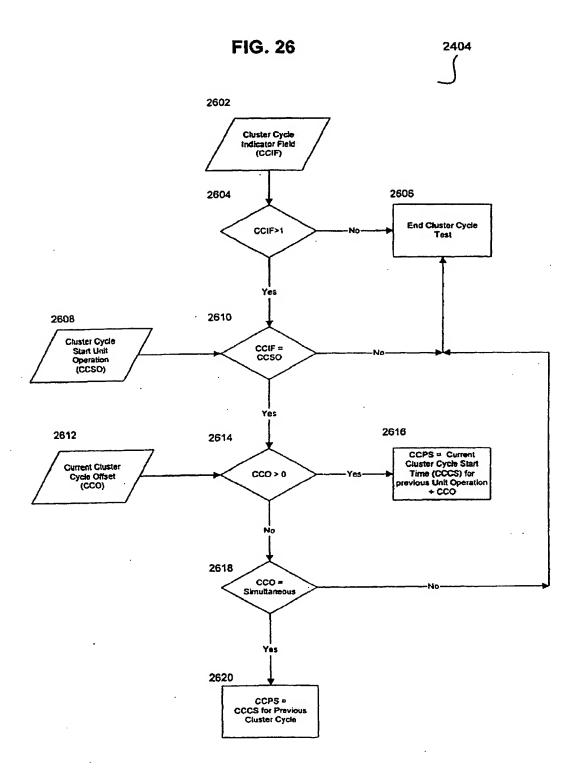
FIG. 24



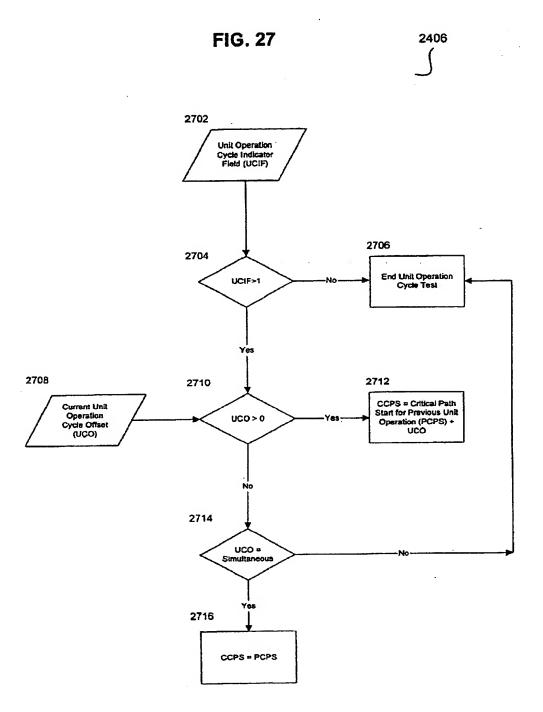
Γitle: The Use of Sub (Partial) Cycles, ...



Γitle: The Use of Sub (Partial) Cycles, ...



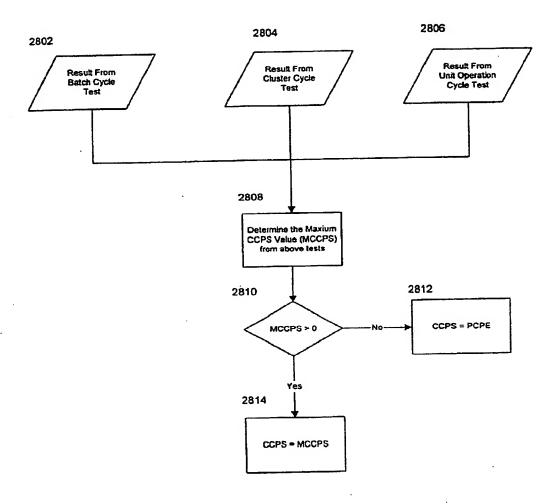
Γitle: The Use of Sub (Partial) Cycles, ...



Title: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown

inventor:

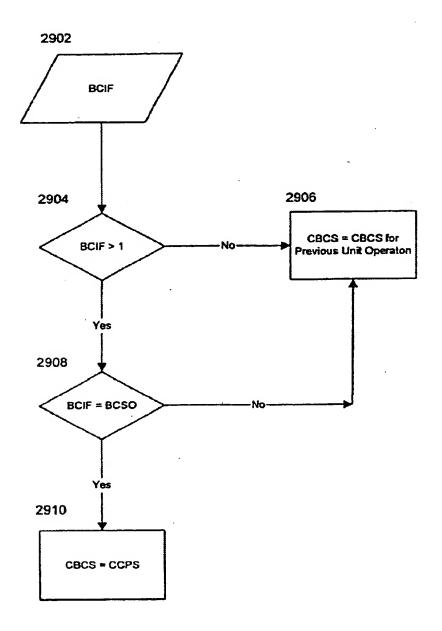
FIG. 28



Docket No.: 3714.1000-000

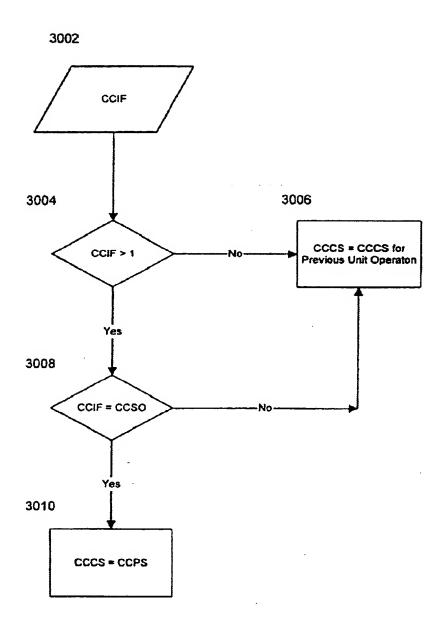
Γitle: The Use of Sub (Partial) Cycles, ...

FIG. 29



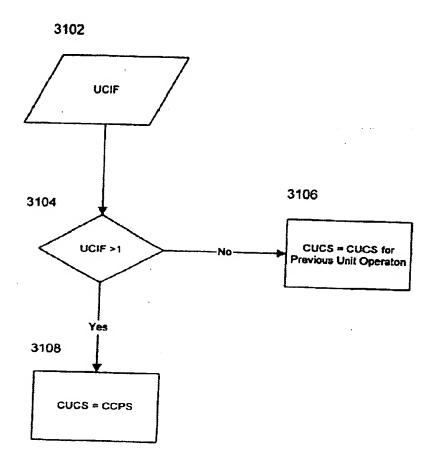
Fitle: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown

FIG. 30



Title: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown

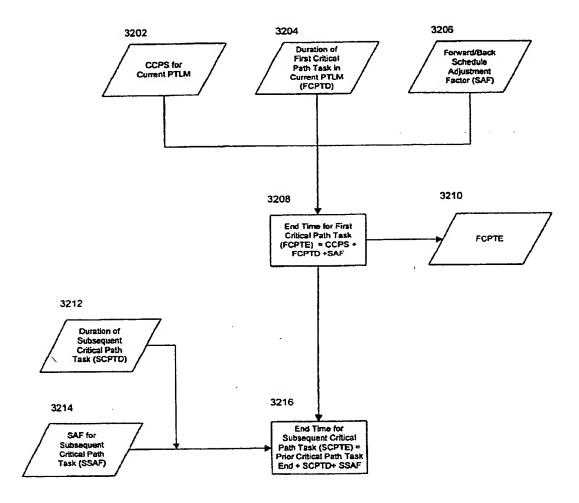
FIG. 31



Docket No.: 3714.1000-000 Title: The Use of Sub (Partial) Cycles, ...

Peter G. Brown Inventor:

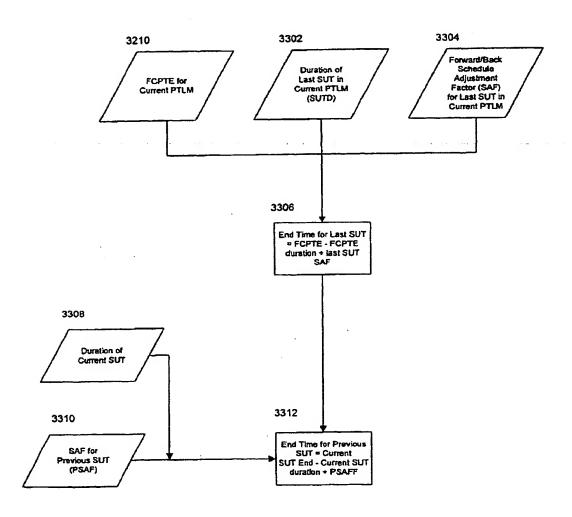
FIG. 32



Docket No.: 3714.1000-000

Title: The Use of Sub (Partial) Cycles, ...

FIG. 33

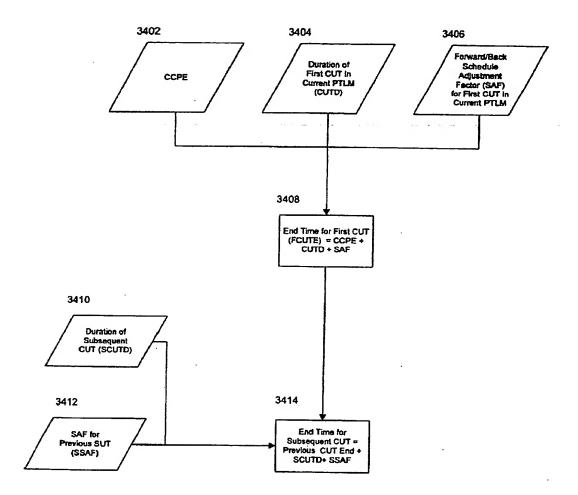


Title: The Use of Sub (Partial) Cycles, ...

Inventor:

Peter G. Brown

FIG. 34



Docket No.: 3714.1000-000 Title: The Use of Sub (Partial) Cycles, ...

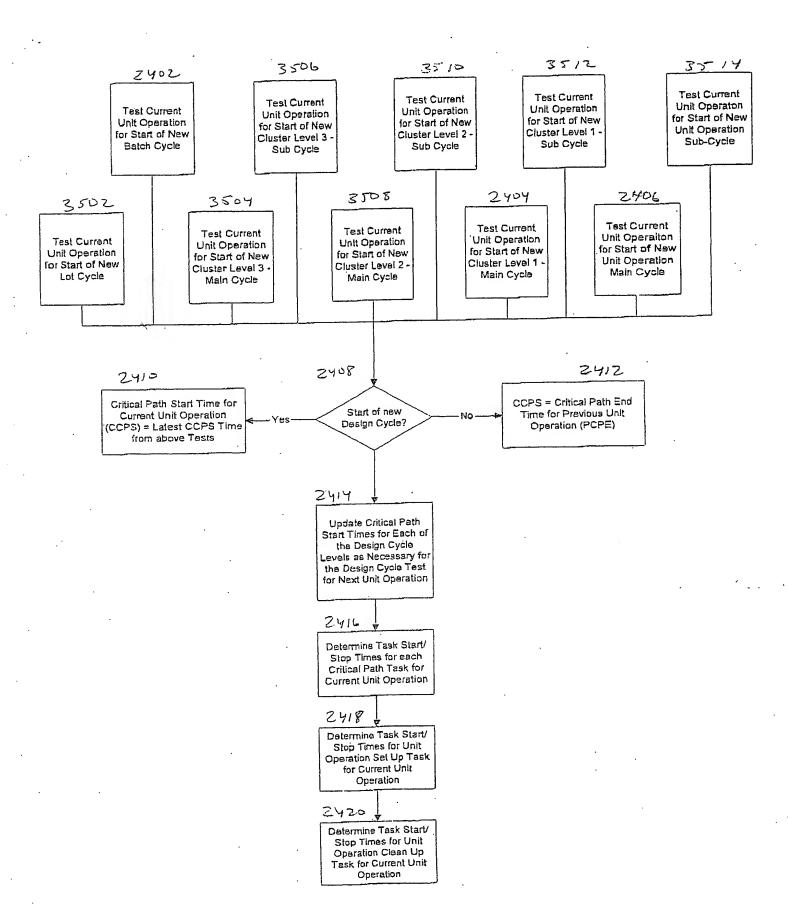
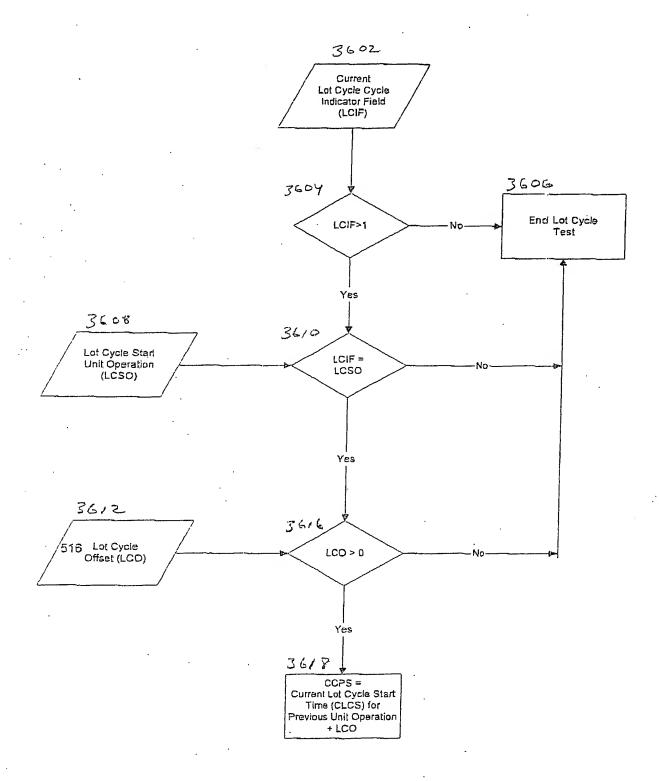
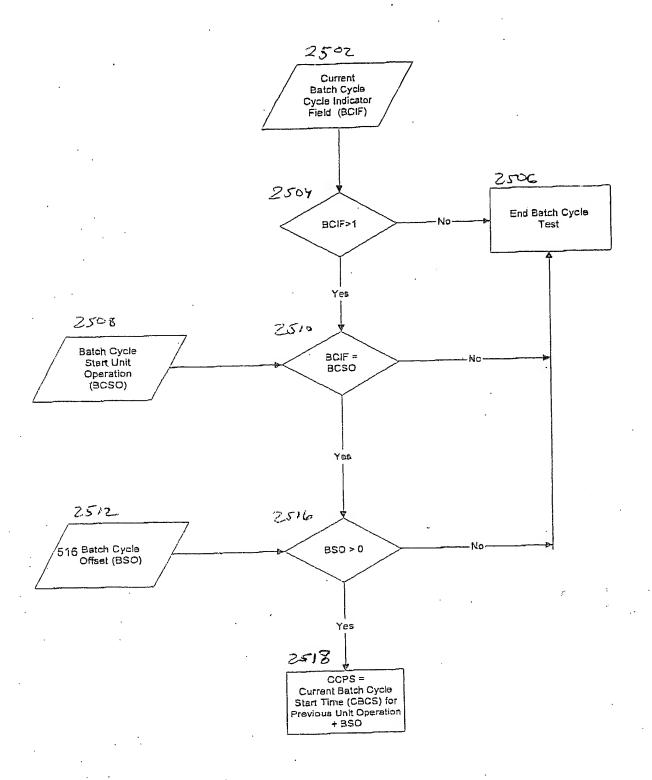


FIG. 35

Title: The Use of Sub (Partial) Cycles, ...

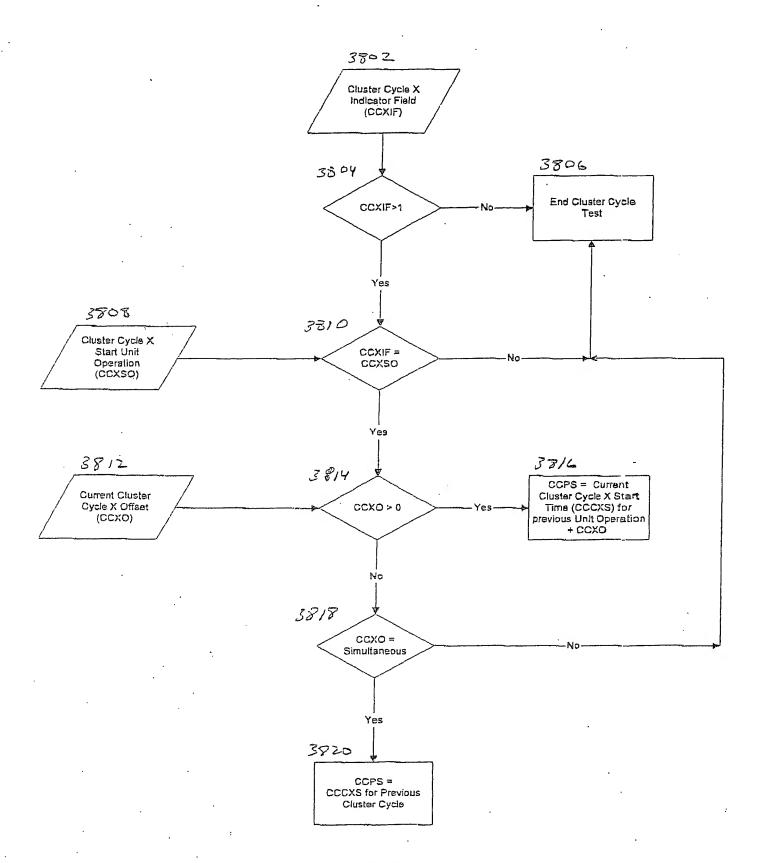


Title: The Use of Sub (Partial) Cycles, ...



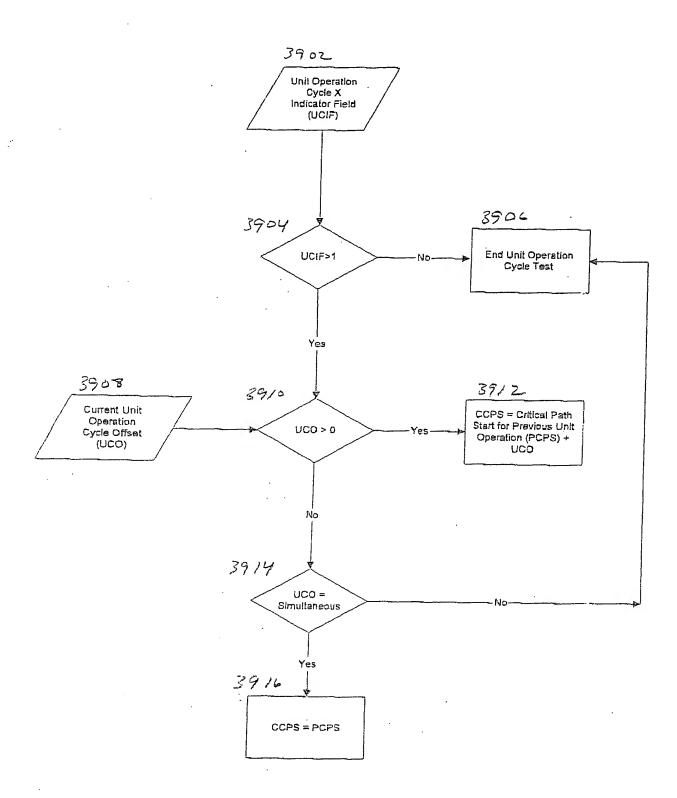
**FIG 37** 

Title: The Use of Sub (Partial) Cycles, ...

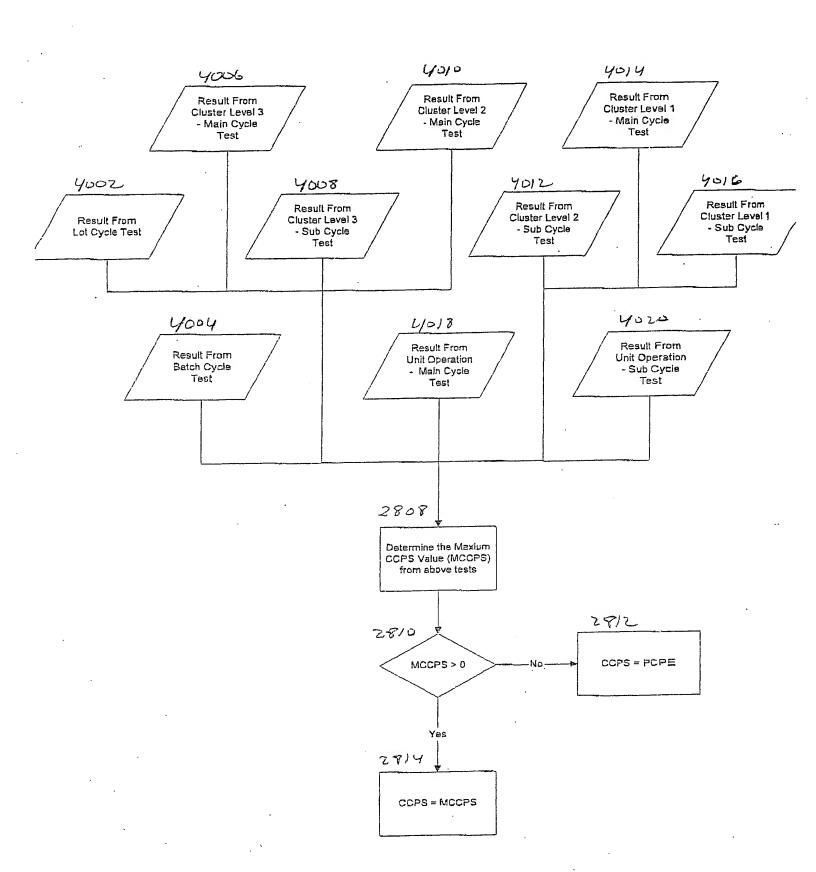


**FIG 38** 

Title: The Use of Sub (Partial) Cycles, ...



Title: The Use of Sub (Partial) Cycles, ...



Title: The Use of Sub (Partial) Cycles, ...
Inventor: Peter G. Brown

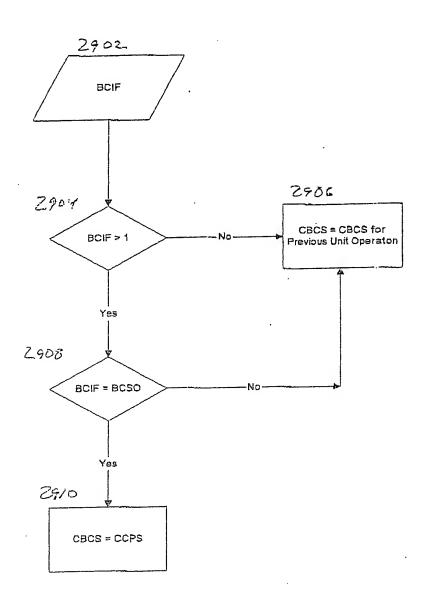
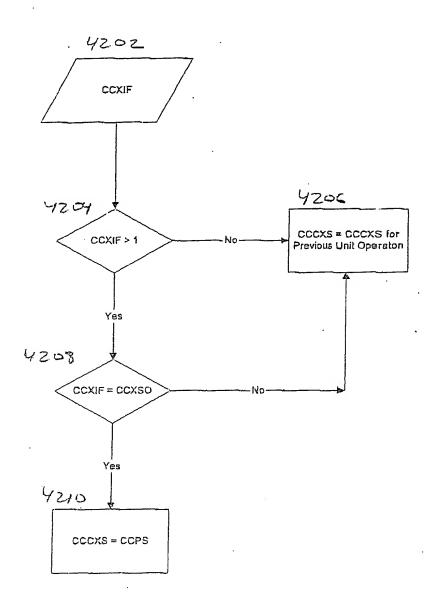
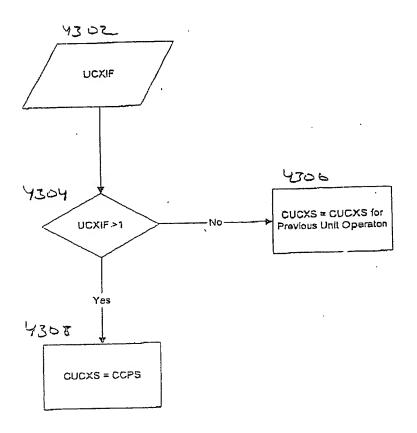


FIG 41

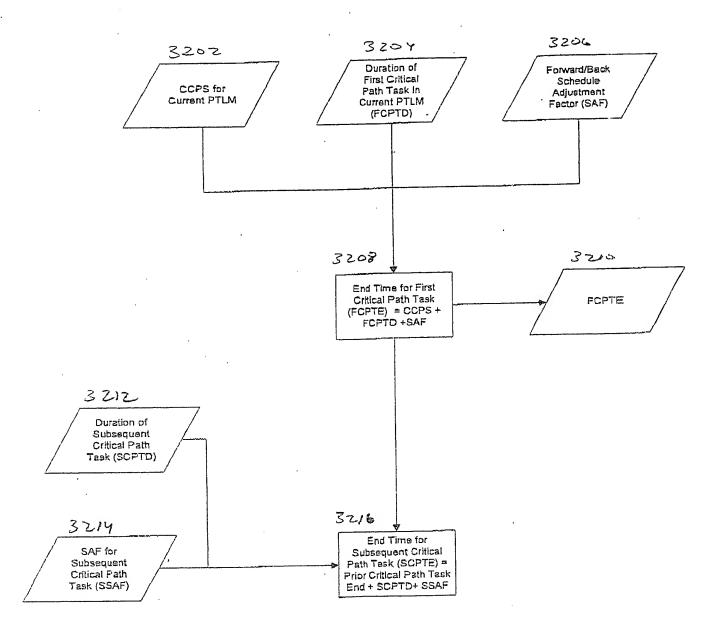
Title: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown



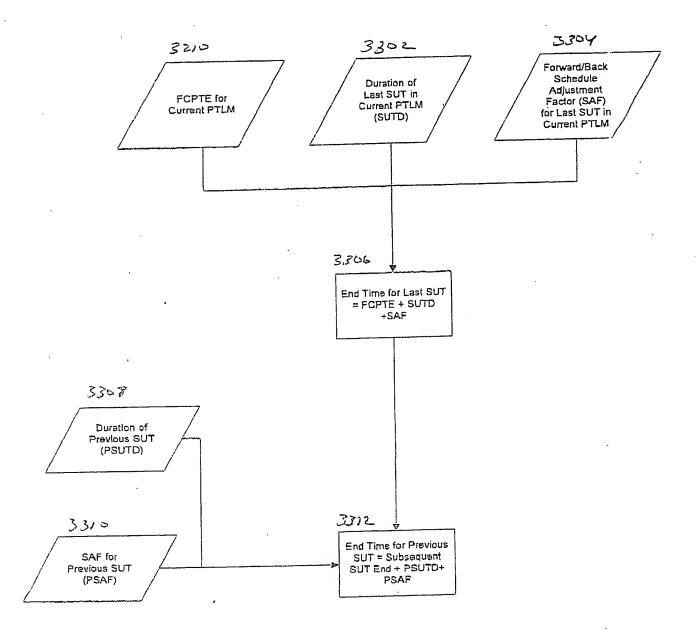
Title: The Use of Sub (Partial) Cycles, ... Inventor: Peter G. Brown



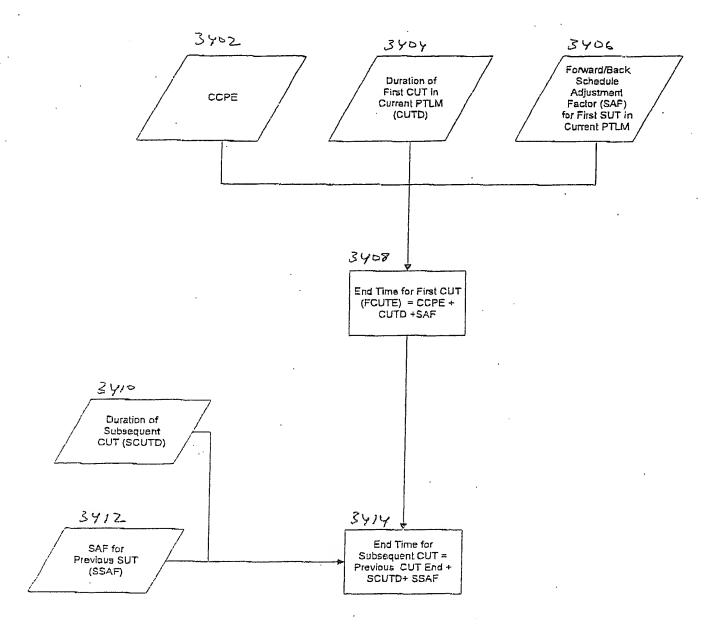
Title: The Use of Sub (Partial) Cycles, ...



Title: The Use of Sub (Partial) Cycles, ...



Title: The Use of Sub (Partial) Cycles, ...



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4786	9	, ,,,,	(Hrs)	Notes											144		144	144	144	<del>1</del> 4	144	144	144	194	144	1	1 4	4	144	144
4784	Lot Cycles/Process Cycle		End	Notes											10315		10315	10315	10315	10315	10315	10315	10315	000	10315	200	10315	10315	10315	10315
4782	Cycles/Pro		Start	Notes											10204		10301	10301	10301	10301	10301	10301	10301	250	10301	200	10301	10301	10301	10301
4780	Lot		Iters.	Notes	-	<del></del>	F	<del>-</del>	<del></del>	= +					<u>ф</u>		10	9	10	5	9	<u></u>	2 9	⊇ :	0 0	2 9	2 5	5 6	9	9
4778			(Hrs)	Notes											72		-62	72	72	72	72	72	2 5	7/	7.2	7 .	3 5	2	72	72
4776	Batch Cycles/Process Cycle	-	$\dashv$	Notes											10315		10315	10315	10315	10315	10315	10315	10315	01501	10315	200	10315	10315	10315	10315
4774	ycles/Proc	-		Notes					·						10204		10301	10301	10301	10301	10301	10301	10301	10501	10301	200	10301	10301	10301	10301
4	atch C		מ כ	ž															_	_	_	_						_	_	_
4772	ä		Iters.	Notes	٠	** *		_	•	- •	<del>.</del>	•	- •		20		2	i &	8	20	8	8 8	8 8	₹ ;	8 8	4 5	3 6	8	×	×
4714			Tag	Notes	10101	10102	10104	10105	10106	0107	010	,,,,,	10201	10203	10204		10301	10302	10303	10304	10305	10306	10307	10308	10309	200	1031	10313	10314	10315
4712 4		i	Stage	Notes					1	_			•				7		_		_				`			_	_	`
4710			Stage ID	Notes	-	<del></del>	- 4-	<del></del>	<del></del>	- +	_	•	۷ ۵	7 0	1 (1)		er.	· Ю	ო	က	ო	က	m 6	ο.	m r	o (	, c	М	က	က
4708				Notes						_																				
4706			Description	Notes	initial Seeding	Spinner Flask Split	Spinner Flask Split	20 L Seed Reactor	80 L Seed Reactor	640 L Seed Reactor	4,000 L Seed Reactor			Production Reactor 1	000000000000000000000000000000000000000			Harvest Cooling to 25 C	,		Protein A Column	Viral Inactivation with HOAc	Adjustment to pH 8.0	0.45 u	0.2 u	Allion Exchange Column	Concernation	Cation Exchange Column	0.2 u Filtration	
4704			Unit Operation (APT)	Notes	lture	Spinner Flask Split - Microcarrier Culture		Stirred Tank Reactor - Microcarrier Seed	Stirred Tank Reactor - Microcarrier Seed	Stirred Tank Reactor - Microcarner Seed	Stirred Lank Reactor - Microcarner Seed	Stage 2		Surred Lank Reactor - Microcarrier Preparation	Harvest/Feed - Microcarrier Production		Stage 3	Outlet Heat Exchange	Cont. Centrifugation - Light Phase Harvest	Tangential Flow - Solids Removal	Prod. Ads. Chromatography - MPLC	Dilution 1 (LD/LP) - Batch	Dilution 1 (LD/LP) - Batch	Microfiltration - Dead End - Solids Removal	Microfitration - Dead End - Solids Removal	Cont. Ads. Crromatography - IMPCC	Ultratitication - Concentration Viality Donates	Prod. Ads. Chromatography - MPLC	Microfiltration - Dead End - Solids Removal	Liquid Storage
4702					-	0.0	o 4	ດ	ω 1	^ '	<b></b>		6 (	2 ;	72		,	. 4	15	16	17	18	9	2	21	77	3 3	25	78	27

302	480 <del>4</del>	7094	2184 486 4812 4814 4816	1810 5	1812 9	1814	9184	4818	48.20	4872
								2	2	
					<del></del>		Process Design Cycles Unit Operation Cyc	ign Cycles	tess Design Cycles Unit Operation Cycles/Cluster Level 1 Cycle	Cycle
							Main Cycles		Sub Cycles	
	Unit Operation (APT)	Description	Code	Stage ID	Stage Inputs	Tag	Iters.	Offset (Hrs)	flers.	Offset (Hrs)
-	Stage 1 Plant Material Milling/Grinding	Grinding of Plant Material		-		10101	-		-	
0 W 4 W @ F	Stage 2 DS Multi-Stage Input Solid/Liquid Extraction Dilution Microfiltration - Dead End - Solids Recovery Resuspension Vacuum Drying - Rotary	Aqueous Extraction Absorbant Addition Absorbed Product Recovery Dissociation of Absorbed Product Vacuum Dry		000000		10201 10202 10203 10204 10205				
1 2 5 4	Stage 3 DS Mutit-Stage Input Morofilitation - Dead End Ultrafilitation - Concentration Microfilitation - Dead End - Solids Removal	Filter Press Product Concentration Product Clarification		пппп	(0)	10301 10302 10304				
15 17 18 19 20 21 22	Stage 4  DS Muti-Stage Input Prod. Ads. Chromatography - MPLC Prod. Ads. Chromatography - MPLC Ultrafiltration - Concentration/Flow Dialysis Prod. Ads. Chromatography - MPLC Microfiltration - Dead End Ultrafiltration - Concentration Lyophilization	Chromatography 1 Chromatography 2 Buffer Exchange Chromatography 3 Sterile Filtration Product Concentration Freeze Dry		444444	4	10401 10402 10403 10404 10405 10406 10407			0 0 - 0	

FIG 48A

Unit Operation (APT)   Hows.   Operation Cluster Lavel 2 Operation (APT)   Hows.   Start Main Operation (APT)   Hows.   Start Main Operation (APT)   Hows.   Start Main Operation (APT)   Hows.   Start Main Operation (APT)   Hows.   Start Main Operation (APT)   Hows.   Start Main Operation (APT)   Hows.   Start Main Operation (APT)   Hows.   Start Main Operation Cluster Lavel 2 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 Operation Cluster Lavel 3 O	2	4802 4804	70G F	3037	Ol 37	2.13+	4814	4816	4818	4810	7855	4824	4826	4828	4830	4832	4834	4.836
Unit Operation (APT)   Lies.   Start   End   Office   Lies   Start   End   Office   Lies   Start   End   Office   Lies   Start   End   Office   Lies   Start   End   Office   Lies   Start   End   Office   Lies   Start   End   Office   Lies   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Color   Col																		
National Milling/Grinding   National Milling Grinding				Unit Oper	ation Clus	ter Level	Cycle/Cl	uster Leve	al 2 Cycle			Unit Ope	ation Clus	ter Level	Cycles/C	uster Leve	J 3 Cycle	
Deparation (APT)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   (Hre)   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   Here.   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   Start   End   Here.   S				Mein	ycles			Subc	ycles			Main	aelay			G day	1	
Adult-Stage Input         2 (10201   10302   12   1   1   1   1   1   1   1   1		Unit Operation (APT)	Iters.	Start	UnOp End	Offset (Hrs)	iters.	UnOp Start	UnOp	Offset (Hrs)	Iters.	UnOp	UnOp	Offset (Hrs)	lters.	UnOp	ChOp	Offse (Hrs.)
With/Stage input         2         10201         10302         12         1         1         1001         10304         24         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1		Stage 1 Plant Material Millng/Grinding	-				-				8	10101		24	-			
Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control Caracteria   Control		Stage 2 DS Mutit-Stage Input Solids Input	2	10201	10302	12	-				6	10101	10304		·			
Wultb-Stage Input         2         10201         10302         12         1         3         10101         10304         24         1           offiltration - Dead End         2         10201         10302         12         1         3         10101         10304         24         1           offiltration - Dead End         Solids Removal         1         1         10304         24         1           offiltration - Dead End - Solids Removal         1         1         10304         24         1           Ads. Chromatography - MPLC         1         1         1         10304         24         1           Ads. Chromatography - MPLC         1         1         1         1         1         1           Ads. Chromatography - MPLC         1         1         1         1         1         1           Ads. Chromatography - MPLC         1         1         1         1         1         1           Ads. Chromatography - MPLC         1         1         1         1         1         1           Ads. Chromatography - MPLC         1         1         1         1         1         1           Ads. Chromatography - MPLC         1		Sollo Liquio Extraction Dilution Microfiltration - Dead End - Solide Recovery Resuspension Vacuum Drying - Rotary		10201 10201 10201 10201	10302 10302 10302 10302 10302	<u> </u>	The second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second secon						10304 10304 10304 10304					
Stage 4  DS Multi-Stage Input Prod. Ads. Chromatography - MPLC Prod. Ads. Chromatography - MPLC Ultrafiltration - Concentration/Flow Dialysis Prod. Ads. Chromatography - MPLC Ultrafiltration - Dead End Ultrafiltration - Concentration Lyophilization		Stag	24 (4)	10201	10302	5 2						10101				<del></del>		1
		Stag					1								-	-		
		OS Multi-Stage Input Prod. Ads. Chromatography - MPLC Prod. Ads. Chromatography - MPLC Ultrafiltration - Concentration/Flow Dialysis Prod. Ads. Chromatography - MPLC Microfiltration - Dead End Ultrafiltration - Concentration Lyophilization					<del></del>				" <del></del>							

Unit Operation (APT)   Part Material Milling/Grinding   Long Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener Cheener	7805	480%	282	780	3 4811	1812	1874	4816	4818	ass.	4922	4824	48%	4828	4830	4832	4834	183
Unit Operation (APT)   Horse   Unit Operation Cluster Lavel 3 Opcies/Batch Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties   Sub-Opties																		
Note   Concentration (APT)   Note   Main Opcies   Start   End (Hrs)   Note   Concentration (APT)   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concentration   Note   Concen				Unit Op	eration C	luster L	yvel 3 Cy	cles/Bat	ch Cycle		Batt	ch Cycles	VProcess (	Cycle	בֿי בֿי	Cycles/Pr	0 88800	ور
Unit Operation (APT)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End   (Hrs)   Items. Start   End				Main	Cycles			SubC	voles									
Stage 1   1000   10405   72   1   1   1   1   1   1   1   1   1		Unit Operation (APT)	Iters.	Unop Start	UnOp End	Offset (Hrs)	fters.		Unop	Offset (Hrs)	fers	UnOp	-	Offset		UnOp	QuO	Offset
Stage 2	1	Stage 1											+	(6)	1618.	LIBIO	2	(¥
DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   Microfiltration - Dead End - Solids Removal   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input   DS Multi-Stage Input		Plant Material Milling/Grinding	2				-											
DS Multi-Stage Input   2   10101   10405   2   10101   10405   2   10101   10405   2   10101   10405   2   10101   10405   3   3   3   3   3   3   3   3   3		Stage 2																
Dilution   Dead End - Solids Recovery   2   10101   10405	~ ~	DS Multi-Stage Input Solid/ Inuid Extraction	C)		10405													
Microfilitation - Dead End - Solids Recovery   2   10101   10405		Ollution Caracilos	~ ~		10405		-	_			- <del>-</del>				- +			
Stage 3		Microfiltration - Dead End - Solids Recovery	2 6		10405										-			
DS Multi-Stage Input		Vacuum Drylng - Rotary	0 0		10405													
DS Multi-Stage Input   Microfiltration - Dead End   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405   10405		Stage 3					•								_			
Ultrafiltration - Concentration   2   10101   10405     Stage 4		DS Multi-Stage Input Microfiltration - Dead End									Ī							
Stage 4  DS Multi-Stage Input Prod. Ads. Chromatography - MPLC Prod. Ads. Chromatography - MPLC Ultrafiltration - Concentration Flow Dialysis Prod. Ads. Chromatography - MPLC Ultrafiltration - Dead End Ultrafiltration - Concentration Lyophilization		Ultrafiltration - Concentration Microfiltration - Dead End - Solids Removal	લલ						<del></del>		<del>*** +** *</del>				<del></del>			
DS Mutit-Stage input Prod. Ads. Chromatography - MPLC Prod. Ads. Chromatography - MPLC Prod. Ads. Chromatography - MPLC Ultrafiltration - Concentration/Flow Dialysis Prod. Ads. Chromatography - MPLC Microfiltration - Dead End Ultrafiltration - Concentration Lyophilization	_	Stage 4							•		_				-			
Ultrafiltration - Concentration/Flow Dialysis 2 10101 10405 Prod. Ads. Chromatography - MPLC 2 10101 10405 Microfiltration - Dead End 1 10405 Ultrafiltration - Concentration 1 1 1		DS Mutti-Stage Input Prod. Ads. Chromatography - MPLC Prod. Ads. Chromatography - MPLC	21 (1) (1)	10101		222												
		Ulitratilitration - Concentration/Flow Dialysis Prod. Ads. Chromatography - MPLC Microfiltration Doctor	a a	10101		2 2 2							·					
		Ultrafiltration - Concentration Lyophilization	<del></del>								- <del></del>							
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FIG 48C

6-3

4970				Offset (Hrs)	Notes																								
4968		ę.	cles	g Pa	Notes						10207	10207	10207										-					_	
4866		atch Cyc	Sub Cycles	UnOp	Notes			T			10205	10205	10205						T					_				•	
4964		Cycles/E		_	Notes			Ι,	- +-		-74	~ ~	~ -	-		-	-		t	= :	-	-	-		_	-	==	=	=
4962		Unit Operation Cluster Level 3 Cycles/Batch Cycle		Offset (Hrs)	Notes				_						-				Ħ										
4		n Clust			┝			_			7.	<u> </u>	-	0	0				1								_		
4960		Operatio	Main Cycles	UnOp End	Notes							10207		10210															
4958		Unit	Mair	UnOp Start	Notes						10205	10205	10205	10209	10209														
4956				Iters.	Notes			<u> </u>	==		· 69	e 0	n	7	~ ~	_	-		T	= -		=			_	-		=	_
4914				Tag	Notes	10101 10102 10103	0105	1	10202	10203	10205	10206	10207	10209	10210	10212	10213	10214	T	1030	10303	10304	10305	10307	10308	10309	10311	10312	10313
4912				Stage Inputs	Notes			-											7									_	
4910				Stage ID	Notes			<del> </del>	4 77	ci c	~~	~ 0	N 60	7	200	(4	7	0 0	T	e .	'n	m	e .	? (r)	က	es (	າຕ	т т	e -
4908					Notes									_					†-										
4906				Description	Notes	0.4L 4.L 4.O.L	4000L		Harvest Cooling to 4 C	Whole Cell Harvest	Slurry Cooling to 4 C	Cell Disruption	Slurry Cooling to 4 C	IB Wash	IB Recovery Solubilization	Clarification	Renaturation	Concentration/Buffer Exchange		of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standard of the standar	HIC Column	Anioin Exchange Column	Viral Inactivation with HOAc	Agustinen to pri a.o. 0.45 บ	0.2 u	Nanofiltration	Concentrations burier exprange HIC Column	Sterile Filtration	
4904				Unit Operation (APT)	Notes		Microbial - Surred Tank Reactor - Seto Fernentation Microbial - Stirred Tank Reactor - Production Fermentation	Stage 2	-	Cont. Centrifugation - Heavy Phase Harvest Dilition 1 of Di. Barch		genization	Cont. Centrifugation - Heavy Phase Harvest		Cont. Centrifugation - Heavy Phase Harvest Dilintion 1 (LDAP) - Barch	t Phase Harvest	-	Tangential Flow - Solids Removal Ultrafiltration - Concentration/Flow Dialysis	Stage 3	Down Stream Multi-Stage Input	- 41-		Dilution 1 (LDALP) - Batch	- Solids Removal		Microfiltration - Dead End - Solids Removal		moval	Liquid Storago
25					<u> </u>	-888	4 ru N 65	Ļ	5 5	8 28					15 26			2 2 2 3 3 3									3 6		
4902	<u> </u>					L					_		_	_		_			L	-, (		.4			.,	.,,			